

PDF issue: 2024-12-13

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(Citation) Enzyme and Microbial Technology, 164:110193

(Issue Date) 2023-03

(Resource Type) journal article

(Version) Accepted Manuscript

(Rights)

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(URL)

https://hdl.handle.net/20.500.14094/0100478478



Caffeic acid production from glucose using metabolically engineered Escherichia coli

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15 Abstract

16 Caffeic acid (3,4-dihydroxycinnamic acid) is a precursor for high-valued compounds with anticancer,

17 antiviral activities, and anti-inflammatory making it an important substance in the food additive,

18 cosmetics, and pharmaceutical industries. Here, we developed an engineered *Escherichia coli* strain

- 19 capable of directly producing high levels of caffeic acid from glucose. Tyrosine ammonia-lyase from
- 20 *Rhodotorula glutinis* (RgTAL) and *p*-coumaric acid 3-hydroxylase from *Saccharothrix espanaensis*
- 21 (SeC3H) were expressed. Next, feedback-resistant chorismate mutase/prephenate dehydrogenase, was

22 introduced to promote L-tyrosine synthesis. This engineered strain CA3 produced 1.58 g/L of caffeic

- 23 acid from glucose without tyrosine supplemented to the medium. Furthermore, to reduce *p*-coumaric
- 24 acid accumulation, 4-hydroxyphenylacetate 3-hydroxylase from *Pseudomonas aeruginosa* (PaHpaBC)
- 25 was introduced. Finally, an engineered strain CA8 directly produced 6.17 g/L of caffeic acid from

26 glucose using a jar fermenter. The *E. coli* developed in this study would be helpful as a chassis strain

- 27 to produce value-added caffeic acid-derivatives.
- 28

29 Keywords: caffeic acid, E. coli, metabolic engineering, shikimate pathway, p-coumaric acid

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31

32 **1. Introduction**

33 Caffeic acid (3,4-dihydroxycinnamic acid) is a type of phenylpropanoid, a naturally occurring organic 34 compound of plant origin. Caffeic acid has pharmacological activities, such as antioxidant [1], 35 antiviral [2], anticancer [3], and antidepressant [4] effects, making it an important substance in the 36 food additive, cosmetics, and pharmaceutical industries. The most common method of its production is 37 extraction, mainly from plants, but the yield is low due to low accumulation in plant cells [5-7], also 38 separation and purification are complicated and inefficient [8]. Therefore, as demand increases, the 39 establishment of more efficient methods is desired, and biosynthesis via metabolically engineered 40 microorganisms is attracting interest as a promising alternative [9]. 41 Escherichia coli is widely used to produce many kinds of chemical compounds. Figure 1 shows the 42 engineered metabolic pathway of caffeic acid biosynthesis in E. coli. Caffeic acid can be synthesized 43 from tyrosine via a two-step reaction by tyrosine ammonia-lyase and p-coumaric acid 3-hydroxylase 44 (C3H). In plants, cinnamic acid is formed from L-phenylalanine by phenylalanine ammonia-lyase,

45 followed by two cytochrome P450 monooxygenases, cinnamic acid 4-hydroxylase (C4H) and *p*-

46 coumaric acid 3-hydroxylase (C3H), which in turn produce *p*-coumaric acid, before it is converted to

47 caffeic acid [10]. However, cytochrome P450 monooxygenases are difficult to express in several

48 microbial systems [11-14]. In microbial systems, sam5-encoded SeC3H (from Saccharothrix

49 espanaensis) can be used, allowing caffeic acid production in Escherichia coli [15,16]. Other effective

50 hydroxylase complexes 4HPA3H for caffeic acid synthesis are EcHpaBC (from *Escherichia coli*) [11,

51 17], TtHpaBC (from Thermus thermophilus HB8) [18], RpHpaBC (from Rhodopseudomonas

52 palustris) and PaHpaBC (from Pseudomonas aeruginosa) [19,20]. They have been reported, to show a

53 high affinity for *p*-coumaric acid.

54

55 Previously, studies have been conducted to synthesize caffeic acid using the precursors *p*-coumaric

acid and L-tyrosine as substrates [16,21]. However, caffeic acid synthesis relying on direct precursor

57 supply is undesirable due to high production costs. Therefore, a production process that allows

58 utilization of a simple carbon source such as glucose has been developed [12, 16]. The reported caffeic

- 59 acid titer using glucose as a carbon source is 1.03 g/L in Escherichia coli [22], 7.92 g/L in a 5-L
- 60 fermenter using *Escherichia coli* [23] and 5.5 g/L in *Saccharomyces cerevisiae* [24, 25].
- 61

62 This study constructed caffeic acid-producing E. coli strain using metabolically engineering 63 techniques. We previously developed a CFT1 strain [26,28], useful for aromatic compound 64 biosynthesis via the shikimate (SHK) pathway. Therefore, it was selected as the parent strain. To 65 construct the caffeic acid synthesis pathway, RgTAL (from Rhodotorula glutinis) and SeC3H (from 66 Saccharothrix espanaensis) were expressed using plasmids. Next, to construct a series of processes to produce caffeic acid from glucose, *tyrA^{fbr}*, encoding a feedback-resistant chorismate 67 68 mutase/prephenate dehydrogenase, was introduced. Constructed tyrosine overproducing strain CA3 69 produced 1.58 ± 0.09 g/L of caffeic acid at a yield of 0.08 ± 0.00 g/g-glucose. Strain CA8, in which 70 PaHpaC (from *Pseudomonas aeruginosa*) was additionally introduced for pathway enhancement, 71 produced 3.61 ± 0.10 g/L of caffeic acid at a yield of 0.19 ± 0.01 g/g-glucose, which significantly 72 increased productivity. Furthermore, strain CA8 was cultured in a bioreactor and produced 6.17 ± 0.19 73 g/L of caffeic acid in 90 hours of culture. The production volume and yield obtained in this study are 74 the highest values reported in previous caffeic acid biosynthesis studies. They may even be applicable 75 in studies involving ferulic acid and L-dopa, which are caffeic acid derivatives.

76

77 2. Materials and Methods

78 2.1 Strains and plasmids construction

The strains and plasmids used in this study are listed in Table 1. ATCC31882 and its derivative
strains were used for caffeic acid production. NovaBlue competent cells (Novagen, Cambridge, MA,
USA) were used for gene cloning. Polymerase chain reaction was performed using KOD FX Neo
(TOYOBO, Osaka, Japan). Custom DNA oligonucleotide primers were synthesized by Invitrogen
Custom DNA Oligos (Thermo Fisher Scientific, Tokyo, Japan) and are listed in Table S1. Codonoptimized foreign gene fragments RgTAL, SeC3H, PaHpaB, and PaHpaC were synthesized by

85 Invitrogen GeneArt Gene Synthesis service (Thermo Fisher Scientific).

86 Plasmids named pZE12-RS, pTrcHisB-RS, pHLA-RS, and pSAK-RS were prepared. Briefly, RgTAL 87 gene fragment was amplified by PCR using the primer pair pZS-RgTAL Fw and pZS-RgTAL Rv 88 with the RgTAL synthetic gene as a template. SeC3H gene fragment was amplified by PCR using the 89 primer pair pZS-SeC3H Fw and pZS-SeC3H Rv with SeC3H synthetic gene as a template. The 90 amplified fragments were cloned between the KpnI/HindIII site of pZE12-MCS or pSAK [27] and the 91 resulting plasmids were designated pZE12-RS or pSAK-RS. RgTAL-SeC3H gene fragment was 92 amplified by PCR using the primer pairs pTrc-RgTAL Fw and pTrc-SeC3H Rv, pHLA-RgTAL Fw 93 and pHLA-SeC3H Rv with pZE12-RS as a template. The amplified fragment was cloned between the 94 Bg/II/EcoRI site of pTrcHisB or between the Bg/II/XhoI site of pHLA [28] and the resulting plasmids 95 were designated pTrcHisB-RS or pHLA-RS. 96 Plasmids named pSAK-BC, pSAK-B, and pSAK-C were prepared as follows. Briefly, PaHpaB gene 97 fragment was amplified by PCR using the primer pair pS-PaHpaB Fw and pS-PaHpaB Rv with 98 PaHpaB synthetic gene as a template. PaHpaC gene fragment was amplified by PCR using the primer 99 pair pS-PaHpaC Fw and pS-PaHpaC Rv with PaHpaC synthetic gene as a template. The plasmids 100 obtained by cloning the PaHpaBC, PaHpaB, and PaHpaC fragments between the KpnI/HindIII sites of 101 pSAK, respectively, were designated pSAK-BC, pSAK-B, and pSAK-C, respectively. pSAK-aroG^{fbr} and pSAK-tktA were prepared as follows. Briefly, *aroG^{fbr}* was amplified by PCR using 102 103 the primer pair pS-aroG^{fbr} Fw and pS-aroG^{fbr} Rv with *aroG^{fbr}* synthetic gene as a template. *tktA* was 104 amplified by PCR using the primer pair pS-tktA Fw and pS-tktA Rv with ATCC31882 genomic DNA as a template. The plasmids obtained by cloning the $aroG^{fbr}$ or *tktA* fragments between the 105 KpnI/HindIII sites of pSAK were designated pSAK-aroG^{fbr} or pSAK-tktA. 106 107 A plasmid for *pheA* gene disruption named $pT\Delta pheA$ was constructed as follows. Briefly, pTargetF 108 [25] served as a template and was amplified by PCR of linearized fragments using the primer pairs 109 del pheA.N20 Fw and del pheA.N20 Rv. The amplified fragments were self-ligated, and the 110 resulting plasmid was designated pTF Δ pheA. The upstream and downstream DNA sequences of *pheA* 111 were amplified using the primer pairs del pheA.UP Fw and del pheA.UP Rv, del pheA.DOWN Fw 112 and del pheA.DOWN Rv with ATCC31882 genome DNA as template. The amplified fragments were

- 113 cloned into the EcoRI/HindIII site of pTF Δ pheA, and the resulting plasmid was designated pT Δ pheA. 114pTApheA::P_{A1lacO1}-PaHpaB was constructed as follows. Briefly, pSAK-B served as a template and 115 was amplified by PCR using the primer pairs del pheA.pSAKinsert Fw and 116 del pheA.pSAKinsert Rv. The resulting fragment was cloned between the Spe I sites of pT_ΔpheA and 117 the resulting plasmid was designated pTApheA::PAllacOl-PaHpaB. pTApheA::PAllacOl-PaHpaC, 118 $pT\Delta pheA::P_{A1|acO1}$ -aro G^{fbr} , and $pT\Delta pheA::P_{A1|acO1}$ -tktA were constructed by the same procedure. Disruption of trpE, pheA, pykA and pykF and transduction of tyrA^{fbr}, PaHpaB, PaHpaC, aroG^{fbr} and 119 120 *tktA* were performed using the CRISPR-CAS9-plasmid system [29] with the following pT Δ trpE, pT Δ pheA, pT Δ pykA, pT Δ pykF, pT Δ trpE::P_{trc}-tyrA^{fbr}, pT Δ trpE::P_{A1lacO1}-tyrA^{fbr} [26, 30], 121 $pT\Delta pheA::P_{A1lacO1}$ -PaHpaB, $pT\Delta pheA::P_{A1lacO1}$ -PaHpaC, $pT\Delta pheA::P_{A1lacO1}$ -aroG^{fbr}, and $pT\Delta$ 122 123 pheA::P_{Allaco1}-tktA. The deletion strains were constructed according to previous report [31]. 124 125 2.2 Medium 126 LB medium (10 g/L tryptone, 5 g/L yeast extract, and 5 g/L NaCl) was used for pre-culture and 127 culture during strain genetic manipulation. M9Y medium (20 g/L glucose, 5 g/L yeast extract, 40 mg/L 128 L-tryptophan, 40 mg/L L-phenylalanine, 0.5 g/L NaCl, 1 g/L NH4Cl, 3 g/L of KH2PO4, 6.7 g/L of 129 Na₂HPO₄, 2.78 mg/L FeSO₄ • 7H₂O, 14.7 mg/L CaCl₂ • 2H₂O, 246 mg/L MgSO₄ • 7H₂O, 10 mg/L of 130 thiamine hydrochloride, 0.1 mM IPTG, 100 mg/L of ampicillin (and 30 mg/L of chloramphenicol)) 131 was used for the caffeic acid production. The medium for bioreactor culture contained 50 g/L glucose. 132 If needed, 0.5 g/L of L-tyrosine was added in the culture medium. 133 134 2.3 Culture conditions 135 E. coli colonies from LB plates were inoculated into test tubes containing 5 mL of LB medium and 136 preincubated at 37°C for 24 h with shaking at 220 rpm. For test tube scale incubation, test tubes 137 containing 5 mL of M9Y medium were inoculated with the pre-culture solution to an OD_{600} of 0.10, 138 incubated at 37°C at 220 rpm, and 300 µL of the solution was collected at 24 and 48 h, which was then
- 139 centrifuged at 10000 rpm for 20 min, and the supernatant was analyzed. For bioreactor cultures, 5 mL

of the pre-cultures in LB medium were transferred into flasks with 20mL of fresh medium and incubated at 37°C for an additional 8 h with shaking at 220 rpm. The pre-culture solution was then inoculated into a bioreactor containing 500 mL of M9Y medium to an OD₆₀₀ of 0.10, incubated at 37°C. The pH was maintained at 7.00 by the automated addition of 28% (v/v) NH₃. Foam formation was suppressed using KM-70 (Shin-Etsu Chemical, Co., Ltd., Tokyo, Japan). Dissolved oxygen was maintained at >20% by controlling agitation. The solution (300 µL) was collected every predetermined time up to 96 h.

147

148 2.4 Analytical methods

149 Cell proliferation was evaluated using a UVmini-1240 spectrophotometer (Shimadzu Corporation, 150 Kyoto, Japan) at an optical density of OD₆₀₀. For glucose analysis, a Prominence HPLC System 151 (Shimadzu Corporation) equipped with a Shodex SUGAR KS-801 column (particle size 6 μ m, L \times 152 I.D. 300×8.0 mm, Shodex) was used. The HPLC profile was monitored using a refractive index 153 detector. Caffeic acid and p-coumaric acid were analyzed using HPLC equipped with a MSII column 154 (particle size 5 μ m, L × I.D. 250 × 4.6 mm, Nacalai Tesque). A two-component solvent system was 155 used. Solvent A was 0.2% phosphate buffer, and solvent B was methanol. The flow rate of the mobile phase was 1.0 mL min⁻¹ and the column was maintained at 40°C. The gradient was started with an 156 157 80:20 mixture of A and B (0-15 min), shifted to a 50:50 mixture of A and B (15-20 min), and back to 158 an 80:20 mixture of A and B (20–25 min). HPLC profiles were obtained using a 240 nm UV–VIS 159 detector. L-Tyrosine was analyzed using HPLC equipped with a PBr column (particle size 5 μ m, L \times 160 I.D. 250×4.6 mm, Nacalai Tesque). A two-component solvent system was used. Solvent A was 0.2% 161 phosphate buffer, and solvent B was methanol. The flow rate of the mobile phase was 1.0 mL min⁻¹ 162 and the column was maintained at 40°C. The gradient was started with 90:10 mixture of A and B (0-6 163 min), shifted to a 50:50 mixture of A and B (6-8 min), and back to 90:10 mixture of A and B (11-13 164 min). HPLC profiles were obtained using a 240 nm (caffeic acid and p-coumaric acid) or 220 nm (L-165 tyrosine) UV–VIS detector. The retention time of caffeic acid, p-coumaric acid and L-tyrosine were 166 4.0 min, 5.0 min and 10.0 min, respectively.

168 **3. Results and Discussion**

169 3.1 Construction of a caffeic acid production pathway in *E coli*

170 The previously developed E. coli CFT1 strain derived from ATCC 31882 was selected as the parent 171 strain for this study. The endogenous phosphotransferase system (PTS) of CFT1 was replaced with a 172 galactose permease/glucokinase system (GalP/Glk system). This modification increased intracellular 173 phosphoenolpyruvate (PEP) utilization, an important factor in aromatic compound biosynthesis. First, 174we generated the CA0 strain based on CFT1 by disrupting *pheA*, which encodes prephenate 175 dehydratase. PheA catalyzes competitive reactions in caffeic acid synthesis such as phenylalanine 176 production. Subsequently, RgTAL and SeC3H were expressed in plasmids to construct a caffeic acid 177 production pathway. Next, RgTAL and SeC3H were cloned into pZE12, pTrcHisB, pHLA, and pSAK 178vectors to create plasmids pZE12-RS, pTrcHisB-RS, pHLA-RS, and pSAK-RS. pZE12, pTrcHisB and 179 pHLA are high-copy plasmids carrying LlacO1 promoter, Trc promoter and HCE promoter. pSAK is a 180 low-copy plasmid carrying A1lacO1 promoter. These plasmids were respectively transformed into 181 CA0. The caffeic acid conversion capacity of each strain was evaluated by adding 0.5 g/L of L-182 tyrosine to the medium. The results of the cultivation are shown in Figure 2. A strain CA0 harboring 183 pZE12-RS showed the highest caffeic acid conversion capacity $(0.47 \pm 0.02 \text{ g/L})$ from L-tyrosine. The 184 amount of p-coumaric acid was less than 0.1 g/L in all strains (data not shown). It indicates LlacO1 185 promoter was suitable for expression of RgTAL and SeC3H. Thus, pZE12-RS was selected as the 186 plasmid for RgTAL and SeC3H expression. All of the following experiments were performed without 187 the addition of tyrosine.

188

189 3.2 Production from glucose by $tyrA^{fbr}$ overexpression

190 Caffeic acid production using the strain CA0 harboring pZE12-RS was only observed when L-tyrosine

191 was added. This strain did not produce caffeic acid from glucose (data not shown). This suggests that

192 the amount of intracellular L-tyrosine must be increased to produce caffeic acid from glucose.

193 Therefore, to promote L-tyrosine synthesis, $tyrA^{fbr}$, encoding feedback-resistant chorismate

194 mutase/prephenate dehydrogenase, was introduced into the CA0 strain in three ways. A low-copy

plasmid for *tyrA^{fbr}* expression under the Trc promoter (pSAK-Ptrc-tyrA^{fbr}) control, was constructed. A 195 CA0 strain harboring pZE12-RS and pSAK-Ptrc-tyrA^{fbr} was named CA1. A strain in which tyrA^{fbr} was 196 197 integrated into the *trpE* locus of the genome under the Trc promoter named CA2 and a strain in which tvrA^{fbr} was introduced into the same locus under the AllacO1 promoter was named CA3. Caffeic acid 198 199 production after 48 h using glucose as a sole carbon source is shown in Figure 3. All strains introduced with $tvrA^{fbr}$ successfully produced caffeic acid from glucose. Particularly, CA3 produced 1.58 ± 0.09 200 201 g/L, approximately 1.3-times more than strains CA1 and CA2. Therefore, CA3 was selected as the 202 caffeic acid producing strain.

203

204 3.3 Enhancement of the caffeic acid production pathway by PaHpaB and PaHpaC overexpression 205 After CA3 cultivation, the accumulation of p-coumaric acid $(1.20 \pm 0.10 \text{ g/L})$, caffeic acid precursor, 206 was observed (Figure 3). This suggests that the reaction to convert *p*-coumaric acid to caffeic acid is 207 the bottleneck of caffeic acid production. We attempted to enhance the reaction that converts p-208 coumaric acid to caffeic acid, however, additional expression of SeC3H could not improve caffeic acid 209 production (data not shown). Other than SeC3H (from Saccharothrix espanaensis), EcHpaBC (from 210 Escherichia coli) and TtHpaBC (from Thermus thermophilus HB8) have been reported to catalyze this 211 reaction. EcHpaBC has high activity than TtHpaBC [18], and EcHpaBC-mediated caffeic acid 212 producing pathway produced 12.1 mg/L of caffeic acid from glucose [11]. When yeast was used as a 213 host, 569.0 mg/mL of caffeic acid was produced [24]. We focused on PaHpaBC (from Pseudomonas 214 aeruginosa), which showed high oxidation activity [19], but they have not previously been used for 215 the production of caffeic acid from glucose. Therefore, we introduced them into CA3. A CA3 strain 216 expressing PaHpaBC and using plasmid pSAK-PaBC was named CA4. A strain CA5, with PaHpaB 217 introduced into the genome of CA3 under the control of the A1lacO1 promoter, was also constructed. 218 A strain CA6 is a CA3 strain carrying plasmid pSAK-PaB for PaHpaB expression only. Similarly, a 219 CA7 strain was constructed by introducing PaHpaC in its genome under the control of the A11acO1 220 promoter, and a CA8 strain carries a plasmid pSAK-PaC for HpaC expression. The results of the 221 culture are shown in Figure 4. CA4, which has PaHpaBC introduced as a complex, showed a slight 222 production decrease, while CA5-CA8, which had PaHpaB/PaHpaC independently introduced, showed

223 decreased p-coumaric acid accumulation and increased caffeic acid production. Particularly, CA8 224produced 3.61 ± 0.09 g/L of caffeic acid, approximately 2.3-times more than CA3. CA7 produced 3.11 225 g/L of caffeic acid, which is higher than CA6 (1.88 g/L) and CA5 (1.91 g/L). The accumulation of p-226 coumaric acid were less than 0.6 g/L among all strains (Figure 4) and no L-tyrosine was detected in 227 the medium (data not shown). Strains CA7 and CA8 overexpressed PaHpaC and CA5 and CA6 228 overexpressed PaHpaB. SeC3H is a single-component FADH₂-utilizing hydroxylases and FAD is 229 regenerated such as a flavin reductase in E. coli [32]. PaHpaBC are a two-component flavin-dependent 230 monooxygenase consists of reductase (PaHpaC) and oxygenase (PaHpaB) [33]. Generally, 231 optimization of FADH₂ transfer within or between flavin-dependent enzymes is important to decrease 232 the extravagant consumption of reducing agents NADH. From the Figure 4, the enhancement of 233 reduced flavin supply (i.e. PaHpaC overexpression) improved caffeic acid production. 234 235 3.4 Enhancement of upstream pathways related to E4P/PEP 236 After caffeic acid biosynthesis pathway was established in E. coli through metabolic engineering of 237 the downstream pathway after chorismic acid, we focused on enhancing the upstream pathway to

238 achieve even higher caffeic acid production. The methods of shikimate pathway enhancement have 239 been reported previously [27]. The first step of the SHK pathway is the condensation of erythrose 4-240 phosphate (E4P) and PEP to produce 3-deoxy-d-arabinoheptulosonic acid 7-phosphate (DAHP) by the 241 action of DAHP synthase. DAHP synthase of E. coli is composed of three isozymes, AroF, and 242 AroH, whose activity is strictly regulated by allosteric regulation and transcriptional repression [35]. Therefore, to enhance DAHP synthesis response, *aroG^{fbr}*, encoding feedback-resistant AroG, was 243 244 introduced into CA8 to create a CA9 strain. Furthermore, the CA8 strain shortened the intermediate 245 substrates, E4P and/or PEP. Therefore, to promote E4P supply, the CA10 strain was generated by

introducing *tktA*, which encodes a transketolase that catalyzes the E4P synthesis reaction, into CA8. In

a report, PEP accumulation can be effectively controlled by the inactivation of pyruvate kinase I

248 (*pykF*)/pyruvate kinase II (*pykA*), which catalyzes the reaction that converts PEP to pyruvate [35, 36].

- 249 Therefore, we generated a CA11 strain, which had *pykF/pykA* disrupted. Since the inactivation of
- 250 pyruvate kinase I/pyruvate kinase II weakens the TCA cycle and affects bacterial growth, 2 g/L of

- sodium pyruvate was added to the culture medium. The results of the cultivation are shown in Figure
- 252 5. Caffeic acid production was almost at similar levels among these strains, suggesting that E4P and
- 253 PEP supply is not a limiting factor in caffeic acid production from glucose.
- 254
- 255 3.5 Caffeic acid production using a jar fermenter
- The CA8 strain was cultured in a jar fermenter to demonstrate the potential for scaled-up production for industrialization. Modified M9Y medium with 50 g/L glucose was used. Figure 6 shows the culture profiles in the jar fermenter. Caffeic acid production using jar fermenter was 6.17 ± 0.19 g/L after 90 h cultivation, which is the highest titer from glucose reported to date. Almost all glucose was consumed during caffeic acid production. Less than 0.6 g/L of p-coumaric acid accumulated, but it was consumed during the cultivation. These results indicates that the caffeic acid-producing strains developed in this study are effective and have the potential to be scaled-up for industrialization.
- 263

4. Conclusion

We succeeded in constructing a caffeic acid-producing pathway from glucose in *E. coli* by metabolic engineering. We demonstrated that enhancement of PaHpaC expression effectively increased caffeic acid production. Using a jar fermenter, we succeeded in producing 6.17 g/L caffeic acid, the highest value obtained from glucose as a carbon source using *E. coli*. We believe that establishing the caffeic acid production process can serve as an effective platform technology for the synthesis of derivatives of other shikimate pathway intermediates.

271

272 Funding

273 This work was supported by the JST-Mirai Program (Grant Number JPMJMI17EI), Japan (to S.N. and

- 274 T.T.), the Japan Society for the Promotion of Science (JSPS) Grant-in-Aid for Scientific Research (A)
- 275 (Grant Number 20H00321), Japan (to T.T.).
- 276

277 **Conflicts of interest**

278 The authors declare no commercial or financial conflict of interest.

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280 Acknowledgments

281 The authors would like to thank Enago (www.enago.jp) for the English language review.

282

283 CRediT authorship contribution statement

- 284 Kosuke Sakae: Conceptualization, Methodology, Investigation, Writing-Original Draft. Daisuke
- 285 Nonaka: Investigation. Mayumi Kishida: Investigation. Yuuki Hirata: Investigation. Ryosuke
- 286 Fujiwara: Methodology, Investigation, Writing–Review & Editing. Akihiko Kondo: Methodology.
- 287 Shuhei Noda: Conceptualization, Methodology, Writing–Review & Editing. Tsutomu Tanaka:
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- 289

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403 Figures



405 Figure 1. Metabolic engineering of caffeic acid producing E. coli. The blue X indicates disruption of 406 the *ptsH*, *ptsI*, *trpE* and *pheA* genes. Red or orange shows genes involved in caffeic acid synthesis 407 overexpressed by plasmid or genomic integration. G6P, glucose 6-phosphate; PEP, 408 phosphoenolpyruvate; E4P, erythrose 4-phosphate; DAHP, 3-deoxy-d-arabinoheptulosonic acid 7-409 phosphate; PP pathway, pentose-phosphate pathway; SHK pathway, shikimate pathway; RgTAL, 410 tyrosine ammonia-lyase from Rhodotorula glutinis; SeC3H, p-coumaric acid 3-hydroxylase from 411 Saccharothrix espanaensis; PaHpaBC, hydroxylase complexes 4HPA3H from Pseudomonas 412 aeruginosa; tyrA^{fbr}, feedback-resistant chorismate mutase/prephenate dehydrogenase; galP, dgalactose transporter; glk, glucokinase; ptsH, phosphocarrier protein HPr; ptsI, phosphoenolpyruvate-413 414 protein phosphotransferase; *pykF*, pyruvate kinaseI; *pykA*, pyruvate kinaseII; *tktA*, transketolase; $aroG^{fbr}$, feedback-resistant 3-deoxy-7-phosphoheptulonate synthase; trpE, anthranilate synthase 415 416 component I; *pheA*, chorismate mutase/prephenate dehydratase. 417





419 Figure 2. Caffeic acid production after 48 h of cultivation in M9Y medium containing 0.5 g/L L-

420 tyrosine and 20 g/L glucose using the strains harboring plasmid pZE12-RS, pTrcHisB-RS, pHLA-RS,

421 or pSAK-RS. The data shown are as the means and standard deviations of three independent

422 experiments.



423

Figure 3. Caffeic acid production after 48 h of cultivation in M9Y medium containing 20 g/L glucose
using strains CA1, CA2, and CA3. The data shown are as the means and standard deviations of three
independent experiments





429 Figure 4. Caffeic acid production after 48 h of cultivation in M9Y medium containing 20 g/L glucose



431 independent experiments.



Figure 5. Caffeic acid production after 48 h of cultivation in M9Y medium containing 20 g/L glucose
using the strains CA8-CA11. The data shown are as the means and standard deviations of three
independent experiments



Figure 6. CA8 culture profiles in a jar fermenter. Blue squares, green triangles, light-brown and darkbrown symbols indicate cell growth, glucose concentration, *p*-coumaric acid concentration and caffeic
acid concentration, respectively. The data shown are as the means and standard deviations of three
independent experiments.

Table 1. Strains and plasmids used in this study.

Strains and Plasmids		
Strains	Genotype	Reference
NovaBlue	endA1 hsdR17(rK12-mK12 ⁺) supE44 thi-1 gyrA96 relA1	Novagen
	<i>lac recA1</i> /F [<i>proAB</i> ⁺ <i>laclqZ</i> Δ <i>M15 Tn10</i> (<i>TetR</i>)]	
ATCC31882	L-Phenylalanine-overproducing strain	ATCC
	(aroF aroG tyrR pheA tyrA trpE)	
CFT1	$ATCC31882\Delta ptsHI::P_{A11acO1}-glk-galP$	Noda et al
CA0	CFT1 <i>\DpheA</i>	This study
CA0/RS	CFT1Δ <i>trpE</i> Δ <i>pheA</i> /pZE12-RS	This study
CA1	CFT1Δ <i>trpE</i> Δ <i>pheA</i> /pZE12-RS+pSAK-Ptrc-tyrA ^{fbr}	This study
CA2	$CFT1\Delta trpE::P_{trc}-tyrA^{fbr}\Delta pheA/pZE12-RS$	This study
CA3	$CFT1\Delta trpE::P_{A1lacO1}-tyrA^{fbr}\Delta pheA/pZE12-RS$	This study
CA4	$CFT1\Delta trpE::P_{A1lacO1}-tyrA^{fbr}\Delta pheA/pZE12-RS+pSAK-BC$	This study
CA5	$CFT1\Delta trpE::P_{A11acO1}-tyrA^{fbr}\Delta pheA::P_{A11acO1}-$	This study
	PaHpaB/pZE12-RS	
CA6	$CFT1\Delta trpE::P_{A11acO1}-tyrA^{fbr}\Delta pheA/pZE12-RS+pSAK-B$	This study
CA7	$CFT1\Delta trpE::P_{A11acO1}-tyrA^{fbr}\Delta pheA::P_{A11acO1}-$	This study
	PaHpaC/pZE12-RS	
CA8	$CFT1\Delta trpE::P_{A11acO1}-tyrA^{fbr}\Delta pheA/pZE12-RS+pSAK-C$	This study
CA9	$CFT1\Delta trpE::P_{A11acO1}-tyrA^{fbr}\Delta pheA::P_{A11acO1}-$	This study
	aroG ^{fbr} /pZE12-RS+pSAK-C	
CA10	$CFT1\Delta trpE::P_{A1lacO1}-tyrA^{fbr}\Delta pheA::P_{A1lacO1}-tktA/pZE12-$	This study
	RS+pSAK-C	
CA11	$CFT1\Delta trpE::P_{A1lacO1}-tyrA^{fbr}\Delta pheA\Delta pykAF/pZE12-$	This study
	RS+pSAK-C	
Plasmids	Characteristic	Reference

pZE12-MCS	$P_{LlacOl}, colE ori, and Amp^r$	Expressys
pTrcHisB	P_{trc} , <i>pBR322 ori</i> , and <i>Amp^r</i>	Life
		lechnologies
pHLA	P_{HCE} , colE1 ori, and Amp^r	Tanaka et al.,
		2011
pSAK	$P_{A11acO1}$, SC101 ori, and Cm^r	Noda et al.,
		2017
pZE12-RS	pZE12 containing RgTAL and SeC3H	This study
pTrcHisB-RS	pTrcHisB containing RgTAL and SeC3H	This study
pHLA-RS	pHLA containing RgTAL and SeC3H	This study
pSAK-RS	pSAK containing RgTAL and SeC3H	This study
pSAK-Ptrc-tyrA ^{fbr}	$pSAK-P_{trc}$ containing $tyrA^{fbr}$	Fujiwara et al.,
		2020
pSAK-BC	pSAK containing PaHpaBC	This study
pSAK-B	pSAK containing PaHpaB	This study
pSAK-C	pSAK containing PaHpaC	This study
pSAK-aroG ^{fbr}	pSAK containing aroG ^{fbr}	This study
pSAK-tktA	pSAK containing <i>tktA</i>	This study
pTargetF	Constitutive expression of sgRNA	Addgene
pCas	Constitutive expression of cas9 and inducible expression	Addgene
	of λ RED and sgRNA	
pT∆trpE	Constitutive expression of sgRNA with donor editing	Fujiwara et al.,
	template DNA for <i>trpE</i> disruption	2020
$pT\Delta trpE::P_{trc}-tyrA^{fbr}$	Constitutive expression of sgRNA with donor editing	Fujiwara et al.,
	template DNA for P_{trc} -tyr A^{fbr} into trpE gene loci	2020
pT∆trpE::P _{A1lacO1} -	Constitutive expression of sgRNA with donor editing	Fujiwara et al.,
tyrA ^{fbr}	template DNA for $P_{A1lacO1}$ -tyr A^{fbr} into trpE gene loci	2020

pT∆pykA	Constitutive expression of sgRNA with donor editing	Noda et al.,
	template DNA for <i>pykA</i> disruption	2016
pT∆pykF	Constitutive expression of sgRNA with donor editing	Noda et al.,
	template DNA for <i>pykF</i> disruption	2016
pT∆pheA	Constitutive expression of sgRNA with donor editing	This study
	template DNA for <i>pheA</i> disruption	
pT∆pheA::P _{A1lacO1} -	Constitutive expression of sgRNA with donor editing	This study
PaHpaB	template DNA for <i>P</i> _{AllacOl} -PaHpaB into <i>pheA</i> gene loci	
pT∆pheA::P _{A1lacO1} -	Constitutive expression of sgRNA with donor editing	This study
РаНраС	template DNA for $P_{A1lacOI}$ -PaHpaC into pheA gene loci	
$pT\Delta pheA::P_{A1lacO1}$ -	Constitutive expression of sgRNA with donor editing	This study
aroG ^{fbr}	template DNA for $P_{A1lacO1}$ -aro G^{fbr} into pheA gene loci	
$pT\Delta pheA::P_{A1lacO1}$ -	Constitutive expression of sgRNA with donor editing	This study
tktA	template DNA for $P_{A1lacO1}$ -tktA into pheA gene loci	

Graphical abstract

