

PDF issue: 2025-12-05

Metabolic Engineering of Shikimic Acid-Producing Corynebacterium glutamicum From Glucose and Cellobiose Retaining Its Phosphotransferase System Function and Pyruvat…

Sato, Naoki Kishida, Mayumi Nakano, Mariko Hirata, Yuuki Tanaka, Tsutomu

(Citation)

Frontiers in Bioengineering and Biotechnology, 8:569406-569406

(Issue Date) 2020-09-10

(Resource Type) journal article

(Version)

Version of Record

(Rights)

© 2020 Sato, Kishida, Nakano, Hirata and Tanaka. This is an open-access article distributed under the terms of the Creative Commons

Attribution License (CC BY). The use, distribution or reproduction in other forums is permitted, provided the original author(s) and the copyright owner(s) are credited a...

(URL)

https://hdl.handle.net/20.500.14094/90007537





Metabolic Engineering of Shikimic Acid-Producing Corynebacterium glutamicum From Glucose and Cellobiose Retaining Its Phosphotransferase System Function and Pyruvate Kinase Activities

Naoki Sato, Mayumi Kishida, Mariko Nakano, Yuuki Hirata and Tsutomu Tanaka*

Department of Chemical Science and Engineering, Graduate School of Engineering, Kobe University, Kobe, Japan

OPEN ACCESS

Edited by:

Yu Wang, Tianjin Institute of Industrial Biotechnology (CAS), China

Reviewed by:

Jian-Zhong Liu, Sun Yat-sen University, China Ralf Takors, University of Stuttgart, Germany

*Correspondence:

Tsutomu Tanaka tanaka@kitty.kobe-u.ac.jp

Specialty section:

This article was submitted to Synthetic Biology, a section of the journal Frontiers in Bioengineering and Biotechnology

Received: 04 June 2020 Accepted: 19 August 2020 Published: 10 September 2020

Citation:

Sato N, Kishida M, Nakano M, Hirata Y and Tanaka T (2020) Metabolic Engineering of Shikimic Acid-Producing Corynebacterium glutamicum From Glucose and Cellobiose Retaining Its Phosphotransferase System Function and Pyruvate Kinase Activities. Front. Bioeng. Biotechnol. 8:569406. doi: 10.3389/fbioe.2020.569406 The production of aromatic compounds by microbial production is a promising and sustainable approach for producing biomolecules for various applications. We describe the metabolic engineering of Corynebacterium glutamicum to increase its production of shikimic acid. Shikimic acid and its precursor-consuming pathways were blocked by the deletion of the shikimate kinase, 3-dehydroshikimate dehydratase, shikimate dehydratase, and dihydroxyacetone phosphate phosphatase genes. Plasmid-based expression of shikimate pathway genes revealed that 3-deoxy-D-arabino-heptulosonate 7-phosphate (DAHP) synthase, encoded by aroG, and DHQ synthase, encoded by aroB, are key enzymes for shikimic acid production in C. glutamicum. We constructed a C. glutamicum strain with aroG, aroB and aroE3 integrated. This strain produced 13.1 g/L of shikimic acid from 50 g/L of glucose, a yield of 0.26 g-shikimic acid/gglucose, and retained both its phosphotransferase system and its pyruvate kinase activity. We also endowed β-glucosidase secreting ability to this strain. When cellobiose was used as a carbon source, the strain produced shikimic acid at 13.8 g/L with the yield of 0.25 g-shikimic acid/g-glucose (1 g of cellobiose corresponds to 1.1 g of glucose). These results demonstrate the feasibility of producing shikimic acid and its derivatives using an engineered C. glutamicum strain from cellobiose as well as glucose.

Keywords: shikimic acid, shikimate pathway, Corynebacterium glutamicum, metabolic engineering, beta-glucosidase, cellobiose

INTRODUCTION

Shikimic acid is a valuable hydroaromatic compound. It is a key metabolic intermediate in the shikimate pathway, a common route for the biosynthesis of a range of aromatic compounds. Shikimic acid possesses a highly functionalized six-carbon ring with three asymmetric centers, and is therefore, a useful precursor for the synthesis of products such as pharmaceuticals, antibiotics,

antithrombotic agents, and vitamins (Rawat et al., 2013; Martinez et al., 2015; Candeias et al., 2018; Kogure and Inui, 2018). This compound has been used as a starting material for the industrial synthesis of oseltamivir phosphate, otherwise known as the anti-influenza drug Tamiflu (Díaz Quiroz et al., 2014). Shikimic acid is also an important starting material for the synthesis of anticancer drugs such as (+)-zeylenone (Liu et al., 2004). Current industrial production of shikimic acid primarily involves its extraction from the seeds of the Chinese star anise plant (almost 80% or more), *Illicium verum*, and subsequent chemical synthesis (Bochkov et al., 2012; Ghosh et al., 2012; Rawat et al., 2013). However, these processes are complex and incur problems such as limitations of raw material and high costs.

The production of biomolecules using microorganisms has recently attracted considerable attention because of the potential for relatively rapid, cost-effective, low-pollution production of industrially important compounds. Shikimic acid is of particular interest due to its importance in a range of industrial applications (Rawat et al., 2013; Martinez et al., 2015; Noda and Kondo, 2017). Microbial production of shikimic acid has several advantages: low-cost renewable feedstocks are readily available in large quantities; the system is environmentally friendly; and high yields can be obtained. Shikimic acid is produced via the shikimate pathway, which is ubiquitous in bacteria, plants, and fungi. This pathway begins with the condensation of phosphoenolpyruvate (PEP) and D-erythrose 4-phosphate (E4P), catalyzed by 3-deoxy-Darabino-heptulosonate-7-phosphate (DAHP) synthetase. DAHP is converted to 3-dehydroquinate (DHQ) by DHQ synthase. DHS synthase catalyzes the next step to produce 3-dehydroshikimate (DHS), which is then converted to shikimic acid by shikimate dehydrogenase. Metabolic engineering for the production of useful compounds derived from the shikimate pathway, including shikimic acid, has been extensively studied (Jiang and Zhang, 2016; Lee and Wendisch, 2017; Noda and Kondo, 2017; Averesch and Krömer, 2018; Huccetogullari et al., 2019; Braga and Faria, 2020), primarily using Escherichia coli as the host strain. A typical strategy for shikimic acid production involves the elimination of the carbon flow from shikimate to chorismite by deletion of the shikimate kinase gene and the reinforcing of carbon flux from glycolysis into the shikimate pathway by overexpression of the shikimate pathway enzymes, including a feedback-resistant DAHP synthase (Gu et al., 2017). Improvement of PEP and E4P availability is another key issue for shikimic acid production. Deletion of pyruvate kinase, inactivation of the phosphotransferase system (PTS) and the redirection of carbon flux from pyruvate to PEP by PEP synthase expression have all been utilized (Chandran et al., 2003). Combining these metabolic approaches, Rodriguez et al. (2013) engineered a shikimic acid-producing E. coli strain, which achieved production of 43 g/L of shikimic acid at a yield of 43% (mol/mol) from glucose in a batch fermenter. However, the inactivation of PTS or pyruvate kinase often causes growth defects, and a laboratory-based adaptive evolution process is required to recover cell growth (Flores et al., 2005, 2007). Introduction of alternative glucose transporter Glf from Zymomonas mobilis with an additional copy of glucokinase from

Z. mobilis could recover cell growth without applying an adaptive evolution experiment (Chandran et al., 2003). Another concern about pyruvate kinase and/or PTS deletion is the shortage of pyruvate supply. For the synthesis of various plant polyphenols such as flavonoids and stilbenoids, pyruvate and acetyl-CoA are important precursor as well as chorismic acid followed by shikimic acid synthesis (Kogure and Inui, 2018).

Corynebacterium glutamicum is a Gram-positive nonpathogenic bacterium, which is already widely used for the industrial production of amino acids such as L-glutamate and L-lysine (Hirasawa and Wachi, 2017; Ikeda, 2017; Baritugo et al., 2018; Becker et al., 2018; Cheng et al., 2018; D'Este et al., 2018; Pérez-García and Wendisch, 2018; Wendisch et al., 2018), and aromatic amino acids such as L-phenylalanine and L-tyrosine (Ikeda, 2006; Zhang C. et al., 2015). This microbe is one of the most promising microbial chassis for the bioproduction of a range of chemicals and fuels, including alcohols, diamines, and organic acids. Kogure et al. (2016) achieved a production of 141 g/L of shikimic acid from glucose using the C. glutamicum R strain using growth-arrested cell reactions in fed-batch fermentation. These researchers induced the expression of a heterologous gene encoding a feedback-resistant form of DAHP from E. coli (Ger et al., 1994), as well as shikimate pathway-related genes. In the engineered strain, PTS and the PEP-independent glucose uptake system were also inactivated. Another study described the production of an engineered C. glutamicum strain derived from strain ATCC13032 using CRISPRi system-mediated transcriptional control. This strain produced 7.76 g/L shikimic acid from sucrose in flask cultivation (Zhang et al., 2016). Zhang et al. constructed an engineered strain using ribosome binding site libraries (Zhang C. et al., 2015; Zhao et al., 2020) or the introduction of the archaeal shikimate pathway (Zhang et al., 2015a). The strains produced shikimic acid at 11.3 and 23.8 g/L, respectively, using sucrose as a carbon source.

Lignocellulosic biomass has attracted much attentions as a promising feedstock because it is renewable, inexpensive and abundant (Bhatia et al., 2020; Zhao et al., 2020). Bio-fuels and chemicals produced from lignocellulosic biomass has a potential to develop the sustainable economic growth. However, most microorganisms cannot directly utilize lignocellulosic biomass, and degradation of this material requires expensive and complex steps. To convert cellulose into monomeric sugars such as glucose, enzymetic saccharification procedures involving endoglucanase, exglucanase and beta-glucosidase (BGL) have been required (Khare et al., 2015). After cleaving the cellulose chain in the middle by endoglucanase, then cellobiohydrolases release cellobiose units from the end of the cleaved cellulose. Finally, BGL hydrolyze cellobiose and cello-oligosaccharides to glucose (Davies et al., 2005). The cellobiose and glucose causes product inhibition of BGL activity. To overcome this problem, excess amount of BGL is added to cellulase mediated hydrolysis (Van Dyk and Pletschke, 2012) or simultaneous saccharification and fermentation (SSF) processes (Liu et al., 2019). Other inhibitors such as tannic, gallic, vanillin were able to cause 20-80% BGL inhibition (Ximenes et al., 2011). It was found that amounts of disaccharides existed in the hydrolyzate,

such as cellobiose (Li et al., 2010). Although shikimic acid production from the mixture of glucose, xylose and arabinose were carried out (Kogure et al., 2016), shikimic acid production using cellobiose or cello-oligosaccharides as a carbon source have not yet been used.

In this study, we constructed a high-producing shikimic acid *C. glutamicum* strain by rational metabolic engineering approaches without PTS inactivation, pyruvate kinase disruption, or the introduction of feedback-resistant variants of DAHP synthase. We simply disrupted shikimic acid and its precursor-consuming genes and introduced only endogenous genes related to the shikimate pathway. Our engineered strain produced 13.8 g/L of shikimic acid, a yield of 0.25 (g-shikimic acid/g-glucose). Further, we demonstrated successful shikimic acid production using cellobiose as the sole carbon source. The titer of shikimic acid production was 13.8 g/L with the same yield of glucose.

MATERIALS AND METHODS

Bacterial Strains, Media, and Cultivation Conditions

All bacterial strains and plasmids used in this study are listed in **Table 1**. *C. glutamicum* ATCC13032 and its recombinants were cultivated aerobically at 30° C in Brain Heart Infusion (BHI) medium or defined CGXII minimal medium containing 50 g/L of glucose or cellobiose and 100 mg/L of aromatic amino acids. CGXIIY medium (CGXII medium containing 4 g/L of yeast extract) was used for shikimic acid production. *E. coli* NovaBlue, which was used for recombinant DNA experiments, was routinely cultivated in Luria–Bertani medium (10 g/L peptone, 5 g/L yeast extract, and 10 g/L NaCl) at 37° C. Kanamycin (25 μ g/mL for *C. glutamicum* strains and 50 μ g/mL for *E. coli*) was added when required.

Construction of Plasmids and Strains

The strains and plasmids used in this study are summarized in **Table 1**. All DNA oligonucleotides used in this study are listed in **Supplementary Table S1**. Gene deletion or substitution plasmids were constructed as follows.

For the *aroK* deletion, the upstream and downstream regions were amplified from *C. glutamicum* strain ATCC 13032 by PCR using the primer pairs $\Delta \text{aroK_up_fw}/\Delta \text{aroK_up_rv}$, and $\Delta \text{aroK_down_fw}/\Delta \text{aroK_down_rv}$, respectively. The two fragments were conjugated by overlap PCR using the primer pair $\Delta \text{aroK_up_fw}/\Delta \text{aroK_down_rv}$, and the resulting fragment was ligated into pK18mobsacB digested using *EcoRI/HindIII*. Other plasmids for gene deletion ($\Delta qsuD$, $\Delta qsuB$, $\Delta nagD$, and $\Delta cg2392$) and for point mutation (gnd S361F) were constructed similarly.

We constructed an *aroG*-expressing plasmid under the control of the H36 promoter as follows. A gene fragment encoding *aroG* was amplified by PCR from *C. glutamicum* ATCC13032 using the primer pairs H36_aroG_fw and AroG_re. The fragment was ligated into plasmid pCC-H36-ldcC digested with *BamHI/XhoI*. The resultant plasmid was named pCC-H36-aroG. Other plasmids expressing *aroB*, *qsuC*, *aroE1* and *aroE3* were constructed similarly.

For aroG integration into the $\Delta aroK$ region, the upstream and downstream regions of $\Delta aroK$ were amplified by PCR using the primer pairs aroK up fw/aroK up rv and aroK down fw/aroK down rv. An aroG-expressing cassette with the H36 promoter and rrnB T1T2 terminator was amplified by PCR using pCC-H36-aroG as a template with the primer pairs aroK-H36_fw/aroK_term_re. The three fragments were conjugated by overlap PCR using the primer pair aroK up fw and aroK down rv, and the resulting fragment was ligated into pK18mobsacB digested with EcoRI/BamHI. Other plasmids for genome integration ($\Delta aroK:aroB$, $\Delta pta:aroG$, $\Delta ldh:aroE1$ $and\Delta ldh:aroE3$) were constructed similarly.

All gene deletions, mutations, and integrations of the *C. glutamicum* genome were introduced by homologous recombination and two-step selection using kanamycin resistance to select for plasmid integration and the *sacB* system to counterselect for plasmid excision.

Transformation of C. glutamicum

C. glutamicum was cultured overnight in 5 mL of BHI medium at 30°C. A further 400 μ L of seed culture was inoculated into 50 mL of BHI medium. After incubation at 30°C until OD₆₀₀ reached 0.5, the cell suspension was centrifuged at 4,000 g for 5 min and washed three times with 5mL of 15% (v/v) glycerol before resuspension in 0.5 mL of 15% glycerol. Transformation of C. glutamicum was performed by electroporation with a 2.5-kV, 200- Ω , 25- μ F electric pulse in a 0.2-cm cuvette using a Gene Pulser (Bio-Rad Laboratories, Hercules, CA).

Conditions for Shikimic Acid Production by *C. glutamicum*

A single colony was used as the inoculum for preculture (5 mL BHI medium in test tubes) and was incubated overnight at 30°C with shaking at 220 rpm. Cells were collected by centrifugation at 4,000 g for 2 min and resuspended in 1 mL of CGXII medium supplemented with 100 mg/L of L-phenylalanine, 100 mg/L of L-tyrosine, 100 mg/L of L-tryptophan, and 100 mg/L of p-aminobenzoate. The suspension (400 μ L) was inoculated into 5 ml of CGXII medium or CGXIIY medium containing 50 g/L of glucose and incubated at 30°C with shaking at 220 rpm 72 h.

Analysis of Substrates and Products

Cell growth was determined by measuring the OD600 nm on a UVmini-1240 spectrophotometer (Shimadzu Corporation, Kyoto, Japan). Glucose concentration was analyzed using a Prominence high-performance liquid chromatography (HPLC) system (Shimadzu) equipped with a Shodex SUGAR KS-801 column (6 μm , 300 \times 8.0 mm L \times I.D., Shodex). The column was maintained at 50°C, and water was used as the mobile

phase at a flow rate of 0.8 ml/min. The HPLC profile was monitored using a refractive index detector. The concentration of shikimic acid was determined using HPLC equipped with COSMOSIL PBr column (5 μ m, 4.6 mm \times 250 mm, I.D. \times L, Nacalai Tesque). A 98:2 mixture of 0.2% phosphoric acid and methanol was used as the mobile phase at a flow rate of 1.0 ml/min, and the column was maintained at

 $40^{\circ}\text{C}.$ The HPLC profile was monitored using a UV-VIS detector at 240 nm.

Quantification of NADPH/NADP and NADH/NAD Ratio

Preparation of samples for the analysis of NADPH and NADH was conducted as follows. Precultured *C. glutamicum* was

TABLE 1 | Bacterial strains and plasmids used in this study.

Strains or plasmids	Genotype	Source or reference
Escherichia coli		
Nova Blue	endA1 hsdR17(rK12-mK12+) supE44 thi-I gyrA96 relA1 lac recA1/F' [proAB+ lacIq $Z\Delta M$ 15:Tn10(Tet r)]; used for gene cloning.	Novagen
SCS110	rpsL (Str1) thr leu endA thi-l lacY galK galT ara tonA tsx dam dcm supE44Δ(lac-proAB) [F' traD36 proAB lacIqZ ΔM15]	STRATAGENE
Corynebacterium glutamicum		
ATCC13032	Wild-type strain	ATCC
SA-1	ATCC13032 $+$ Δ cglMRR (cg1996-cg1998), Δ qsuD, Δ qsuB, Δ nagD, Δ aroK	This study
SA-2	$SA-1 + gnd^{S361F}$	This study
SA-3	$SA-2 + aroK:P_{H36}$ -aroG	This study
SA-4	$SA-2 + aroK:P_{H36}-aroB$	This study
SA-5	SA-2 + $aroG^{gtg \rightarrow atg}$, $\Delta cg2392$	This study
SA-6	$SA-5 + aroK:P_{H36}$ -aroB	This study
SA-7	$SA-5 + aroK:P_{H36}$ -aroB, pta: P_{H36} -aroG	This study
SA-8	$SA-7 + \Delta ldh$	This study
SA-9	$SA-7 + Idh:P_{H36}-aroE1$	This study
SA-10	SA-7 + $Idh:P_{H36}$ -aroE3	This study
Plasmids		
pCCS	E. coli–C. glutamicum shuttle vector for control, KmR	Matsuura et al., 2019
pCC-H36-cgR0949-Tfu0937	pCCS derivative carrying sequences encoding the CgR0949 secretion signal fused to <i>T. fusca</i> Tfu0937 under the control of the H36 promoter	Matsuura et al., 2019
pCC-P _{H36} -aroG	pCCS containing aroG under the control of the H36 promoter	This study
pCC-P _{H36} -aroB	pCCS containing aroB under the control of the H36 promoter	This study
pCC-P _{H36} -qsuC	pCCS containing qsuC under the control of the H36 promoter	This study
pCC-P _{H36} -aroE1	pCCS containing aroE1 under the control of the H36 promoter	This study
pCC-P _{H36} -aroE3	pCCS containing aroE3 under the control of the H36 promoter	This study
pCC-P _{H36} -tal-tkt	pCCS containing <i>tal</i> and <i>tkt</i> (cg1774-cg1776, NCgl1512-NCgl1513) under the control of the H36 promoter	This study
pCC-P _{H36} -pck	pCCS containing pck under the control of the H36 promoter	This study
pK18mobsacB	sacB, lacZ, Km ^R , MCS, mobilizable vector, enables selection/counter-selection for integration/excision in <i>C. glutamicum</i>	ATCC
pK18-gnd ^{S361} F	pK18mobsacB derivative for substitution of gnd ^{S361F}	This study
pK18-∆qsuD	pK18mobsacB derivative for qsuD deletion	This study
pK18-∆qsuB	pK18mobsacB derivative for qsuB deletion	This study
pK18-∆nagD	pK18mobsacB derivative for nagD deletion	This study
pK18-∆aroK	pK18mobsacB derivative for aroK deletion	This study
pK18-∆ldh	pK18mobsacB derivative for <i>Idh</i> deletion	This study
pK18- Δ aroK-P _{H36} aroB	pK18mobsacB derivative for insertion of <i>aroB</i> expression cassette under the control of H36 promoter into <i>aroK</i> locus	This study
pK18-∆pta-P _{H36} aroG	pK18mobsacB derivative for insertion of <i>aroG</i> expression cassette under the control of H36 promoter into <i>pta</i> locus	This study
pK18-Δldh-P _{H36} aroE1	pK18mobsacB derivative for insertion of <i>aroE1</i> expression cassette under the control of H36 promoter into <i>Idh</i> locus	This study
pK18-∆ldh-P _{H36} aroE3	pK18mobsacB derivative for insertion of <i>aroE3</i> expression cassette under the control of H36 promoter into <i>Idh</i> locus	This study

inoculated into 5 ml of CGXIIY medium containing 50 g/L of glucose and incubated at 30°C with shaking at 220 rpm for 24 h. The extraction buffer (methanol: chloroform = 7:3) was added to cells and incubated at 1,000 rpm at 4°C overnight. The supernatant was centrifuged at 13,000 g for 5 min and evaporated. The evaporated samples were analyzed using the Enzychrom NADP + /NADPH Assay Kit ECNP-100 (BioAssay Systems, Hayward, United States) and Enzychrom NAD + /NADH Assay Kit E2ND-100 (BioAssay Systems, Hayward, United States) according to the manufacturer's procedures.

Quantification of the Transcriptional Level of mRNA Using Real-Time qPCR

The transcriptional expression of *aroB*, *aroG*, and *ldh* in SA-2, SA-5, and SA-7 was quantified using real-time qPCR. Total RNA was isolated after 24 h of cultivation in CGXIIY medium using a NucleoSpin RNA column (Takara Bio, Shiga, Japan) according to the manufacturer's protocol.

Quantitative real-time qPCR was performed using a LightCycler[®] 96 System (Roche Molecular Systems, Inc., CA, United States) with RNA-directTM Real-time PCR Master Mix (TOYOBO). The primer pairs used are listed in **Supplementary Table 1**. The normalized transcriptional level of each mRNA was calculated using the relative quantification method using the cg3177 (Ncgl2772) gene as the housekeeping gene.

Statistical Analysis

Analysis of variance (ANOVA) was conducted with Honestly Significant Difference (HSD) test by EZR software (Kanda, 2013). The data of shikimic acid are average of 3 biological replicates with error bars representing standard deviation and asterisk indicates significant difference (p < 0.05) from control strain.

RESULTS AND DISCUSSION

Construction of Shikimic Acid-Producing *C. glutamicum*

We used ATCC13032 ΔMRR (a partially prophage-free variant) as the parent strain for constructing shikimic acid-producing C. glutamicum (Bott et al., 2013). We disrupted four genes encoding shikimate kinase aroK (cg1828, NCgl1560); DHS dehydratase qsuB (cg0502, NCgl0407); QA/SA dehydratase qsuD (cg0504, NCgl0409); and DHAP phosphatase nagD (cg2474, NCgl2175), leading to the accumulation of shikimic acid (Figure 1). The strain, called SA-1 (DaroK, DqsuB, DqsuD, and DnagD), exhibited auxotrophy for aromatic amino acids and p-aminobenzoate. Therefore, small amounts of L-phenylalanine, L-tyrosine, L-tryptophan, and p-aminobenzoate (100 mg/L) had to be added to the minimal medium for the strain to grow. No shikimic acid was detected in the parental strain, but SA-1 produced 1.3 \pm 0.04 g/L of shikimic acid in CGXII medium containing 50 g/L of glucose after 72 h of cultivation (Figure 2A). Ohnishi et al. reported that the point mutation Ser361Phe of the 6-phosphogluconate dehydrogenase gene (gnd; cg1643, NCgl1396) increased L-lysine production due to enhancement of NADPH supply (Ohnishi et al., 2005). Shikimate dehydrogenase *aroE* requires NADPH as a cofactor for its enzymatic activity, so we introduced this point mutation into SA-1 by allelic replacement. The resulting strain SA-2 produced 1.9 \pm 0.23 g/L of shikimic acid after 72 h, an increase of approximately 40% over that of SA-1 (**Figure 2A**).

Overexpression of Shikimate Pathway Genes in Strain SA-2 Using a Plasmid-Based Expression Method

To improve shikimic acid production, each gene of the shikimate pathway was overexpressed under the control of the strong synthetic constitutive promoter PH36 (Yim et al., 2013). This promoter has been used to produce recombinant single-chain variable fragment (Yim et al., 2014), gammaaminobutyrate (Choi et al., 2015), and 1,5-diaminopentane (Matsuura et al., 2019; Kim et al., 2020). Key genes located on the C. glutamicum chromosome are DAHP synthase, encoded by aroG (cg2391, NCgl2098); DHQ synthase, encoded by aroB (cg1827, NCgl1559); DHS synthase, encoded by qsuC (cg0503, NCgl0408); shikimate dehydrogenase, encoded by aroE1 (cg1283, NCgl1087); and aroE3 (cg1835, NCgl1567). Although C. glutamicum carries the DAHP synthase encoded by aroF, its contribution to the shikimate pathway is less than that of aroG (Liu et al., 2008), and we did not select it as a candidate. Individual plasmids were created for the overexpression of aroG, aroB, qsuC, aroE1, and aroE3, under the control of the strong constitutive promoter PH36. Each plasmid was introduced into the SA-2 strain, and the strains were cultivated in CGXII medium containing 50 g/L of glucose. Figure 2B shows shikimate production after 72 h of cultivation. SA-2 overexpressing aroG gene (SA-2/aroG) produced 5.4 \pm 0.65 g/L of shikimate, 2.8-times higher than SA-2 (Figure 2A). Overexpression of aroB (SA-2/aroB) also slightly increased shikimate production $(2.3 \pm 0.23 \text{ g/L} \text{ after } 72 \text{ h})$. Overexpression of qsuC, aroE1, and aroE3 did not increase shikimic acid production.

Construction of *C. glutamicum* Strains With Integrated Shikimate Pathway Genes, and Introduction of Additional Shikimate Pathway Genes Using Plasmid-Based Expression

As shown in **Figure 2B**, the enhancement of *aroG* or *aroB* gene expression contributed to the increased production of shikimic acid. We therefore integrated an extra copy of *aroG* or *aroB* under the control of the promoter P_{H36} into the *aroK* locus of the SA-2 genome. The resulting strains were named SA-3 (SA-2/aroK:P_{H36}-aroG) and SA-4 (SA-2/aroK:P_{H36}-aroB), respectively. To enhance the expression of *aroG*, we changed the start codon of *aroG* from "gtg" to "atg" (aroG^{gtg → atg}) with an inframe deletion of *cg2392* (NCgl2099) in SA-2 (**Figure 3D**). The resulting strain was named SA-5 (SA-2/Δcg2392, aroG^{gtg → atg}). Changing the translational start codon of the gene increased its expression (Vogt et al., 2016; Jorge et al., 2017). The *aroG* gene is located downstream of *cg2392*, a predicted exonuclease,

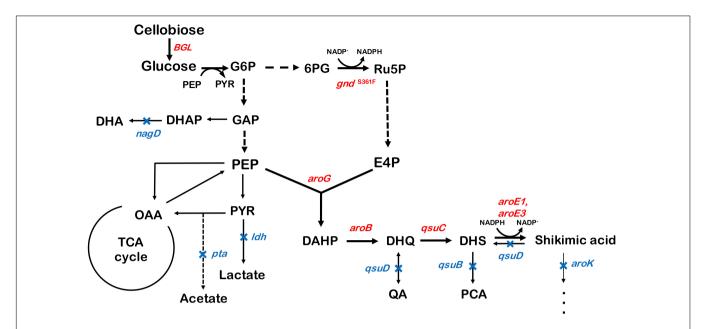


FIGURE 1 | Metabolic engineering of *Corynebacterium glutamicum* for shikimic acid production. The blue X indicates deletion of the *nagD*, *qsuB*, *qsuB*,

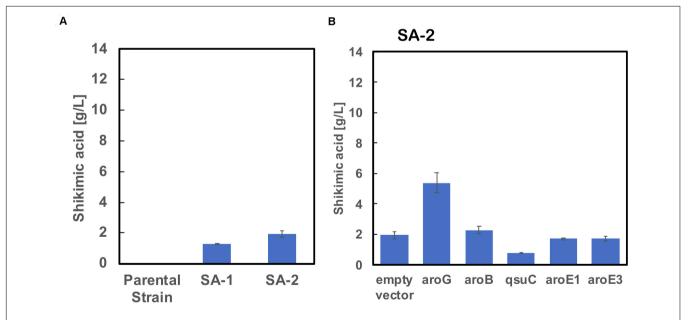


FIGURE 2 | (A) Shikimic acid production titer in strains SA-1 and SA-2 harboring empty vectors. (B) SA production titer in SA-2 harboring each individual shikimate pathway gene expression plasmid. CGXII medium containing 50 g/L of glucose was used as the sole carbon source. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

and they constitute an operon. In-frame deletion of *cg2392* and replacement of *aroG* downstream from the native promoter should increase *aroG* expression. To evaluate the shikimic acid production of SA-3, SA-4, and SA-5, we introduced an empty plasmid and cultivated the strains. **Figures 3A–C** (left bars of each

panel) shows the shikimic acid production of SA-3, SA-4, and SA-5. Using CGXII medium containing 50 g/L of glucose, SA-3, SA-4, and SA-5 strains produced 1.7 \pm 0.30 g/L, 3.0 \pm 0.09 g/L, and 2.4 \pm 0.15 g/L of shikimic acid, respectively. Statistical analysis revealed that significant difference was observed between SA-2

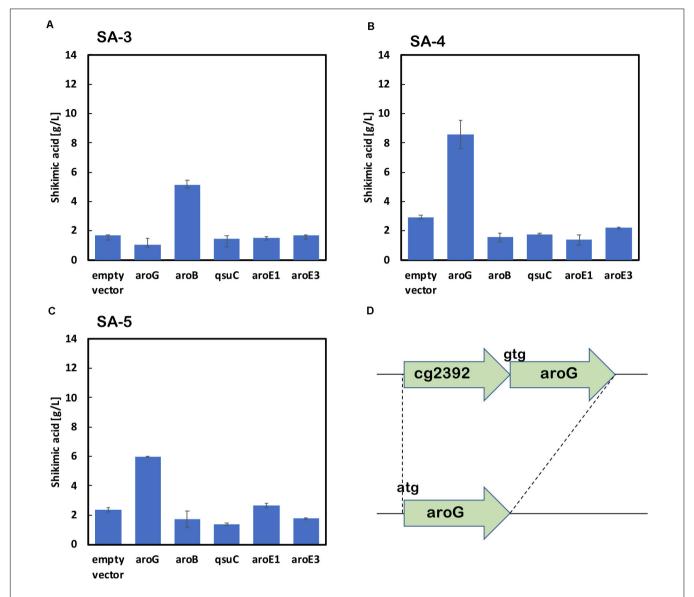


FIGURE 3 | Shikimic acid production titer in strains **(A)** SA-3, **(B)** SA-4, and **(C)** SA-5 harboring each shikimate pathway gene expression plasmid. CGXII medium containing 50 g/L of glucose was used as the sole carbon source. Panel **(D)** illustrates a gene cg2392 deletion and replacement of the start codon in the SA-5 strain. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

and SA-5, SA-3, and SA-5 (**Supporting Figure S1**). Glucose was consumed all strains, and the yield were 0.035 mol/mol (SA-3), 0.062 mol/mol (SA-4), 0.03550 mol/mol (SA-5), respectively. Unlike plasmid-based expression systems (**Figure 2B**), the integration of aroB increased shikimic acid production 1.5-fold over SA-2. In contrast, the integration of *aroG* into strain SA-2 decreased the production of shikimic acid. The SA-5 strain with the modified start codon had increased shikimic acid production by 26% compared with SA-2. These results suggest that *aroG* expression from the integrated *aroG* expression cassette was insufficient for shikimic acid production. In the case of *aroB*, a single integration of the *aroB* gene increased the shikimic acid titer over that of the plasmid-based overexpression system (SA-2/aroB; **Figure 2B**). Although we used medium copy number

plasmid (about 30; Tauch, 2005), these results suggest that the production of large amounts of shikimic acid seems to depend on the plasmid copy number (Hashiro et al., 2019).

Using SA-3, SA-4, and SA-5 as host cells, each shikimate pathway gene aroG, aroB, qsuD, aroE1, and aroE3 were introduced using a plasmid-based expression system. **Figures 3A–C** shows shikimic acid production after 72 h of cultivation. In the case of SA-3 (an aroG-integrated strain), additional plasmid-based aroB gene overexpression (SA-3/aroB) produced 5.1 ± 0.65 g/L of shikimic acid production, three-fold higher than SA-3. In strain SA-4 (an aroB-integrated strain), additional overexpression of aroG (SA-4/aroG) resulted in the highest shikimic acid production, up to 8.6 ± 0.96 g/L in CGXII minimal media containing 50 g/L of glucose. Overexpression of

other genes did not improve shikimate production in either SA-3 or SA-4. The SA-5 strain expressing *aroG* (SA-5/aroG) increased the shikimate titer up to 6.0 ± 0.05 g/L, slightly higher than that of SA-2/aroG (5.4 ± 0.65 g/L; **Figure 2B**).

Construction of *C. glutamicum* Strains With Integrated *aroG* and *aroB* Genes and Cultivation in Nutrient-Rich Media

As shown in Figure 3, aroG and aroB are key genes for high shikimic acid production. Zhang et al. reported that high-level expression of aroG and medium-level expression of aroB using plasmids having different ribosome binding sites were suitable for shikimic acid production (Zhang et al., 2015b). In the engineered strain series developed by Kogure's group, all of the genes of the shikimate pathway were expressed using a plasmid (Kogure et al., 2016). In this study, we introduced an aroB expression cassette into the aroK locus of the SA-5 strain. The resulting SA-6 strain produced 3.3 \pm 0.29 g/L of shikimic acid (data not shown), which was slightly higher than the production of SA-5. We constructed strain SA-7 (SA-2/ $\Delta pta:aroG$, $\Delta aroK:aroB$, $\Delta cg2392$, $aroG^{gtg \rightarrow atg}$) by introducing an extra copy of the aroG gene chromosomally into the pta region of SA-6. The pta locus, encoding phosphate acetyltransferase, was selected for aroG integration to minimize any tendency for the formation of acetate as a byproduct. After cultivation, the SA-7 strain produced 5.7 \pm 0.36 g/L of shikimic acid in CGXII medium containing 50 g/L of glucose (Figure 4, left blue bar), which was three-fold higher than SA-3 and 1.9-fold higher than SA-4. We additionally introduced each shikimate pathway gene

into SA-7. SA-7 overexpressing aroG (SA-7/aroG) produced 8.7 ± 0.23 g/L of shikimic acid (**Figure 4**), almost the same as SA-4/aroG. SA-7 overexpressing aroB (SA-7/aroB) produced 5.0 ± 0.46 g/L of shikimic acid (**Figure 4**), almost the same as SA-4/aroB. These results suggest that a combination of plasmidbased aroG expression and single integration of *aroB* are valuable for high shikimic acid production. We measured the shikimic acid production of SA-7 transformants in nutrient-rich CGXIIY medium (CGXII medium containing 4 g/L of yeast extract and 50 g/L of glucose). Strain SA-7 carrying an empty plasmid produced 10.9 ± 0.92 g/L of shikimic acid (Figure 4, orange bar) with a yield of 0.22 g shikimate/g-glucose, about two-fold higher than SA-7 cultivated in CGXII minimal medium. Graf et al. reported that ATP and NADPH generation was enhanced in nutrient-rich medium (Graf et al., 2018), contributing to increased shikimic acid production. SA-7 overexpressing aroG and aroB strains produced 10.9 \pm 0.38 g/L and 10.6 \pm 0.36 g/L of shikimic acid in CGXIIY medium (Figure 4, orange bars), respectively, almost the same as SA-7 carrying an empty vector. Alternatively, SA-7 carrying plasmids containing qsuC, aroE1, or aroE3 had slightly increased shikimic acid titers of up to 11.3 ± 0.31 , 12.0 ± 1.70 , and 13.5 ± 0.50 g/L, respectively. The one-way ANOVA analysis on the titer of shikimic acid production in CGXIIY medium revealed a statistically significant between empty vector and aroE3. These results indicate aroE3 would be a rate-limiting step.

Feedback inhibition is another concern for shikimic acid production. In *E. coli*, AroG is specifically feedback regulated by L-phenylalanine, AroF and AroH are feedback regulated by L-tyrosine and L-tryptophan, respectively (Martinez et al., 2015).

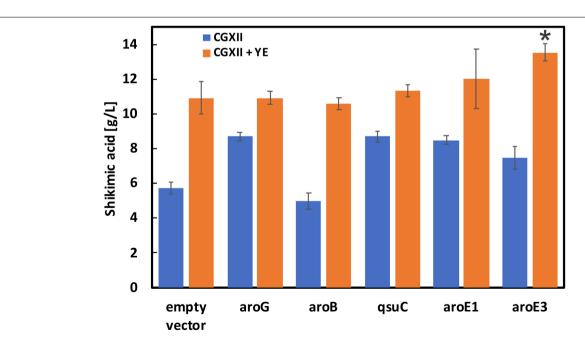


FIGURE 4 | Shikimic acid production titer in SA-7 strains harboring each shikimate pathway gene expression plasmid. Blue bars indicate SA production when the CGXII medium containing 50 g/L of glucose was used as the sole carbon source. Orange bars indicate the CGXIIY medium used. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation. P values were computed using the two-tailed Student's t-test (*P < 0.05; **P < 0.01).

In the case of *C. glutamicum*, AroG activity was decreased only a 10 to 15% under 5 mM of L-phenylalanine and L-tyrosine concentrations (Liu et al., 2008). We also evaluated shikimic acid production CGXIIY medium including 100-fold higher (10 g/L) concentration of L-phenylalanine, L-tyrosine and L-tryptophan. The shikimic acid titer after 72 h was 6.6 \pm 0.12 g/L (data not shown), about 40% decrease. These results suggest that the feedback inhibition of shikimic acid production with 100 mg/L (about 5–6 mM) of these amino acids was a small impact.

The time courses of each strain carrying an empty vector in CGXIIY medium containing 50 g/L of glucose are shown in **Figure 5**. SA-7 produced the highest amount of shikimic

acid (10.9 \pm 0.92 g/L), followed by SA-4, with 8.4 \pm 0.19 g/L. The amount of shikimic acid produced by SA-4 in nutrient-rich CGXIIY medium was 2.8-fold higher than in CGXII minimum medium (**Figure 3B**, left bar). SA-2, SA-3, and SA-4 produced shikimic acid at 2.9 \pm 0.24 g/L, 2.9 \pm 0.04 g/L, and 4.0 \pm 0.36 g/L, respectively, after 72 h in CGXIIY medium. The cell growth of SA-2 and SA-3 was higher than that of SA-7 and SA-4, suggesting that the carbon flux in SA-2 and SA-3 is distributed toward cell growth rather than shikimic acid synthesis. All strains except SA-3 consumed glucose for 48 h. Lactic acid was observed to be a major byproduct (**Figure 4D**). The SA-4 and SA-7 strains accumulated lactic acid at 6.9 \pm 0.85 g/L and 8.3 \pm 0.70 g/L,

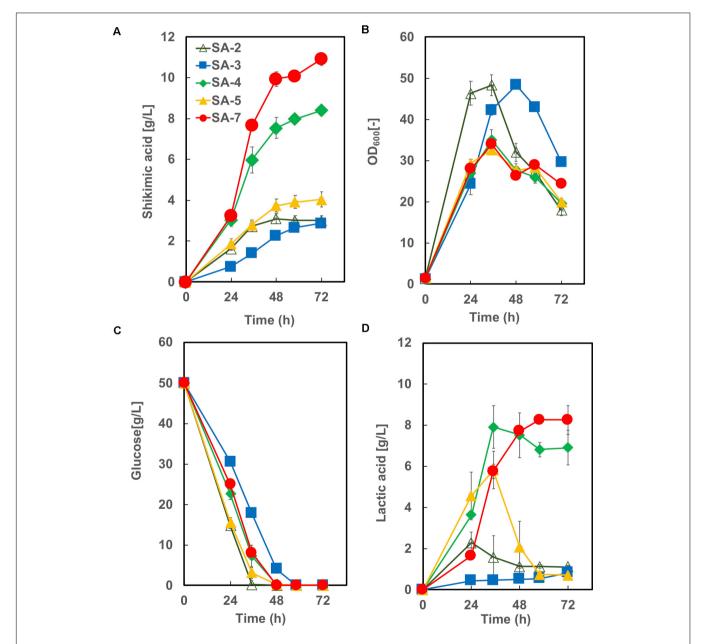


FIGURE 5 | Culture profiles of SA-7 and its derived strains. (A) Shikimic acid production, (B) cell growth, (C) glucose consumption, and (D) lactic acid accumulation. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

respectively. When these strains were cultivated in the CGXIIY medium without glucose, shikimic acid production was less than 0.5 g/L (data not shown). Acetic acid was not detected during cultivation in SA-7 or other strains. 3-dehydroshikimate, reported as a major precursor, was not detected in any strain.

Evaluation of Cofactor Balance and Transcription Levels of the Lactate Dehydrogenase Gene in SA-6

As shown in **Figure 5D**, lactic acid accumulation was a major metabolic byproduct. **Figures 6A,B** show intracellular NADPH/NADP + and NADH/NAD + ratios after 24 h of cultivation in CGXIIY medium. In spite of lactic acid formation, as shown in **Figure 5D**, the NADH/NAD + ratio was almost the same among the parental strains SA-2 and SA-7. The NADPH/NADP + ratio of SA-7 was decreased relative to SA-2 due to the final reaction of shikimic acid synthesis, which is catalyzed by shikimate dehydrogenase, *aroE*. These results are consistent with previous reports (Kogure et al., 2016).

The transcription levels of aroG, aroB, and lactate dehydrogenase gene ldh were evaluated using real-time qPCR after 24 h of cultivation. The aroG levels of the SA-5 strain were slightly increased compared with those of SA-2 (**Figure 6C**), suggesting that a gene cg2391 deletion had little influence on aroG transcription level (**Figure 4D**). Alternatively, in the case of the SA-7 strain, in which aroG and aroB are integrated under the control of the P_{H36} promoter, the transcription levels of aroG and aroB were significantly increased, up to 64.3- and 40.0-fold higher than those of the parental strain, contributing to improved shikimic acid production. The transcription levels of ldh were increased in all strains other than the parental strain. We disrupted the ldh gene (cg3219, NCgl2810) in SA-7. The resulting strain, SA-8, produced 9.9 \pm 0.78 g/L of shikimic acid and accumulated 8.1 \pm 0.18 g/L of lactic

acid (**Supplementary Figure S2**), almost the same as SA-7. *C. glutamicum* has another putative lactate dehydrogenase gene (cg3227, NCgl2817), which might contribute lacate accumulation. A gene *lldD* (cg3227, NCgl2817) encoding quinone-dependent L-lactate dehydrogenase has the ability to utilize lactate as a carbon source (Stansen et al., 2005), however, activation of lactate re-assimilation pathway required a full oxygen supply (Käß et al., 2014). A limited-oxygen condition after glucose depletion in the test tube was another factor for lactate accumulation.

Construction of *C. glutamicum* Strains With Integrated *aroG*, *aroB*, and *aroE3* Genes and Shikimic Acid Production Using Cellobiose as a Carbon Source

Based on the results from Figure 5, we constructed strain SA-9 $(SA-7/\Delta ldh:aroE1)$ and SA-10 $(SA-7/\Delta ldh:aroE3)$ by introducing an extra copy of the aroE1 or aroE3 gene chromosomally into the ldh region of SA-7, respectively. After 72 h cultivation, the SA-9 strain produced 8.5 ± 0.46 g/L of shikimic acid in CGXIIY medium containing 50 g/L of glucose (Figure 7A). Alternatively, SA-10 produced 13.1 \pm 0.25 g/L of shikimic acid with the yield of 0.26 g-shikimic acid/g-glucose (Figure 7A), which was almost same level of SA-7 harboring aroE3 expressing plasmid (Figure 4). We then focused on improving the availability of the shikimate pathway precursors PEP and E4P. To increase the supply of E4P, we constructed a plasmid for the overexpression of the endogenous transketolase (tkt) and transaldolase (tal) genes (cg1774-cg1776, NCgl1512-NCgl1513) and introduced into SA-10. Alternatively, to increase the availability of PEP, a plasmid for overexpression of endogenous phosphoenolpyruvate carboxykinase gene (pck; cg3169, NCgl2765) was introduced into SA-10. The resulting strain produced shikimic acid at 11.2 ± 0.71 g/L and 12.3 ± 0.25 g/L, respectively (**Figure 7B**).

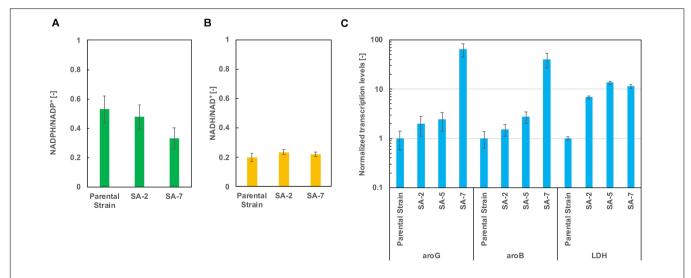


FIGURE 6 | The ratio of (A) NADPH/NADP + and (B) NADH/NAD + after 24 h cultivation in CGXIIY medium. Panel (C) shows the transcription levels of aroG, aroB, and ldh after 24 h of cultivation. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

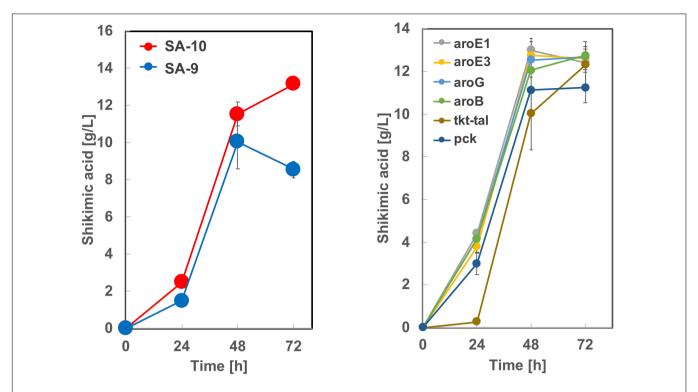


FIGURE 7 | Shikimic acid production titer in (A) SA-9, SA-10 and (B) its derived strains. CGXII medium containing 50 g/L of glucose was used as the sole carbon source. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

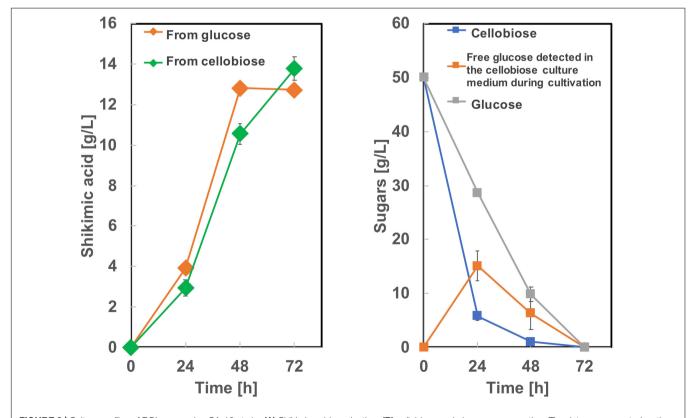


FIGURE 8 | Culture profiles of BGL expressing SA-10 strain. (A) Shikimic acid production, (B) cellobiose and glucose consumption. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

We also introduced *aroB*, *aroG*, *aroE1*, and *aroE3* expression plasmid into SA-10 strain. Each strain produced shikimic acid at 12.8 \pm 0.11 g/L, 12.7 \pm 0.37 g/L, 12.4 \pm 0.34 g/L and 12.6 \pm 0.55 g/L, respectively (**Figure 7B**).

To produce shikimic acid from cellobiose as a carbon source, we used BGL Tfu0937 from Thermobifida fusca YX, which has been shown to exhibit high BGL activity in E. coli (Tanaka et al., 2011) and C. glutamicum (Matsuura et al., 2019). A plasmid secretory expressing BGL (Matsuura et al., 2019) was introduced into SA-10 and cultivated in CGXIIY medium containing 50 g/L of glucose or cellobiose as a carbon source. As shown in **Figure 8**, this BGL-secreting SA-10 strain produced 13.8 \pm 0.56 g/L of shikimic acid from cellobiose as well as 12.7 \pm 0.19 g/L of shikimic acid from glucose. The yield from cellobiose is 0.25 g-shikimic acid/g-glucose (1 g of cellobiose corresponds to 1.1 g of glucose), which was almost same as that from glucose (0.25 g-shikimic acid/g-glucose). These results show BGL expression did not affect shikimic acid production, which are corresponding to previous report (Matsuura et al., 2019). Cellobiose was completely consumed by 72h. However, free glucose was observed in the culture medium at 24 and 48 h cultivation. indicating the conversion of cellobiose into glucose by BGL was sufficient and improvement of glucose uptake might enhance shikimic acid production.

Microbial shikimic acid production has been reported by many groups. An engineered E. coli strain reported by Chandran et al. (2003) produced 87 g/L of shikimic acid from glucose with a yield of 0.36 (mol/mol) in fed-batch fermentation. Rodriguez et al. (2013) reported a metabolically engineered E. coli strain and the strain produced 43 g/L of shikimic acid with the yield of 0.43 (mol/mol) in batch culture. In the case of C. glutamicum, Kogure et al. (2016) reported 141 g/L of shikimic acid production using growth-arrested cell reaction with the yield of 0.51 (mol/mol). In our study, although shikimic acid titer (13.1 g/L) and yield (0.27 mol/mol) were less than those reports, we developed high shikimic acid producing C. glutamicum ATCC13032 strain without loss of PTS function and pyk activity. It should be useful property for the synthesis of plant polyphenols. In addition, we demonstrated direct shikimic acid production from cellobiose, which has the possibility of the reduction of the production cost.

CONCLUSION

In conclusion, The *C. glutamicum* strain SA-10 was metabolically engineered for enhanced shikimic acid production from glucose by optimizing its metabolic pathway, retaining the PTS system and *pyk* activity. Genomic integration of the *aroB*, *aroG* and *aroE3* genes improved shikimic acid production up to 13.1 g/L

REFERENCES

Averesch, N. J. H., and Krömer, J. O. (2018). Metabolic engineering of the shikimate pathway for production of aromatics and derived compounds - present and future strain construction strategies. Front. Bioeng. Biotechnol. 6:32. doi: 10. 3389/fbioe.2018.00032 with a yield of 0.26 g-shikimic acid/g-glucose. Moreover, BGL-expressing SA-10 strain produced shikimic acid from cellobiose with almost same titer and yield from glucose. This study is an important step in developing an economically feasible and sustainable process for shikimic acid production.

DATA AVAILABILITY STATEMENT

The datasets presented in this study can be found in online repositories. The names of the repository/repositories and accession number(s) can be found in the article/ Supplementary Material.

AUTHOR CONTRIBUTIONS

NS and TT proposed the idea, designed the experiments, and wrote the manuscript. NS, MK, MN, YH, and TT performed the experiments. All authors read and approved the final manuscript.

FUNDING

This work was supported by the JST-Mirai Program (Grant Number JPMJMI17EI), Japan to TT, the Japan Society for the Promotion of Science (JSPS) Grant-in-Aid for Scientific Research (B) (Grant Number 19H02526), Japan to TT.

ACKNOWLEDGMENTS

The authors would like to thank Enago (www.enago.jp) for the English language review.

SUPPLEMENTARY MATERIAL

The Supplementary Material for this article can be found online at: https://www.frontiersin.org/articles/10.3389/fbioe. 2020.569406/full#supplementary-material

FIGURE S1 | Culture profiles of strain SA-2, SA-3 and SA-5. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation. P values were computed using the two-tailed Student's t-test (*, P < 0.05).

FIGURE S2 | Culture profiles of strain SA-8. **(A)** Shikimic acid production, **(B)** cell growth, **(C)** glucose consumption, **(D)** lactic acid accumulation. The data are presented as the average of three independent experiments, and error bars indicate the standard deviation.

TABLE S1 | Oligonucleotide primers used in this study.

Baritugo, K. A., Kim, H. T., David, Y., Choi, J. I., Hong, S. H., Jeong, K. J., et al. (2018). Metabolic engineering of Corynebacterium glutamicum for fermentative production of chemicals in biorefinery. Appl. Microbiol. Biotechnol. 102, 3915– 3937. doi: 10.1007/s00253-018-8896-6

Becker, J., Rohles, C. M., and Wittmann, C. (2018). Metabolically engineered Corynebacterium glutamicum for bio-based production of chemicals, fuels,

- materials, and healthcare products. $Metab.\ Eng.\ 50,\ 122-141.\ doi:\ 10.1016/j.\ ymben.2018.07.008$
- Bhatia, S. K., Jagtap, S. S., Bedekar, A. A., Bhatia, R. K., Patel, A. K., Pant, D., et al. (2020). Recent developments in pretreatment technologies on lignocellulosic biomass: effect of key parameters, technological improvements, and challenges. *Bioresour. Technol.* 300:122724. doi: 10.1016/j.biortech.2019.122724
- Bochkov, D. V., Sysolyatin, S. V., Kalashnikov, A. I., and Surmacheva, I. A. (2012). Shikimic acid: review of its analytical, isolation, and purification techniques from plant and microbial sources. *J. Chem. Biol.* 5, 5–17. doi: 10.1007/s12154-011-0064-8
- Bott, M., Noack, S., and Frunzke, J. (2013). Construction of a prophage-free variant of Corynebacterium glutamicum ATCC 13032 for use as a platform strain for basic research and industrial biotechnology. Appl. Environ. Microbiol. 79, 6006–6015. doi: 10.1128/AEM.01634-13
- Braga, A., and Faria, N. (2020). Bioprocess optimization for the production of aromatic compounds with metabolically engineered hosts: recent developments and future challenges. Front. Bioeng. Biotechnol. 8:96.
- Candeias, N. R., Assoah, B., and Simeonov, S. P. (2018). Production and synthetic modifications of shikimic acid. *Chem Rev.* 118, 10458–10550. doi: 10.1021/acs. chemrev.8b00350
- Chandran, S. S., Yi, J., Draths, K. M., von Daeniken, R., Weber, W., and Frost, J. W. (2003). Phosphoenolpyruvate availability and the biosynthesis of shikimic acid. *Biotechnol. Prog.* 19, 808–814. doi: 10.1021/bp025769p
- Cheng, J., Chen, P., Song, A., Wang, D., and Wang, Q. (2018). Expanding lysine industry: industrial biomanufacturing of lysine and its derivatives. J. Ind. Microbiol. Biotechnol. 45, 719–734. doi: 10.1007/s10295-018-2030-8
- Choi, J. W., Yim, S. S., Lee, S. H., Kang, T. J., Park, S. J., and Jeong, K. J. (2015). Enhanced production of gamma-aminobutyrate (GABA) in recombinant Corynebacterium glutamicum by expressing glutamate decarboxylase active in expanded pH range. Microb. Cell Fact 14:21. doi: 10.1186/s12934-015-0205-9
- Davies, G. J., Gloster, T. M., and Henrissat, B. (2005). Recent structural insights into the expanding world of carbohydrate-active enzymes. *Curr. Opin. Struct. Biol.* 15, 637–645. doi: 10.1016/j.sbi.2005.10.008
- D'Este, M., Alvarado-Morales, M., and Angelidaki, I. (2018). Amino acids production focusing on fermentation technologies A review. *Biotechnol. Adv.* 36, 14–25. doi: 10.1016/j.biotechadv.2017.09.001
- Díaz Quiroz, D. C., Carmona, S. B., Bolívar, F., and Escalante, A. (2014). Current perspectives on applications of shikimic acid aminoshikimic acids in pharmaceutical chemistry. Res. Rep. Med. Chem. 4, 35–46. doi: 10.2147/RRMC. S46560
- Flores, N., Flores, S., Escalante, A., De Anda, R., Leal, L., Malpica, R., et al. (2005). Adaptation for fast growth on glucose by differential expression of central carbon metabolism and gal regulon genes in an *Escherichia coli* strain lacking the phosphoenolpyruvate:carbohydrate phosphotransferase system. *Metab. Eng.* 7, 70–87. doi: 10.1016/j.ymben.2004.10.002
- Flores, N., Leal, L., Sigala, J. C., De Anda, R., Escalante, A., Martínez, A., et al. (2007). Growth recovery on glucose under aerobic conditions of an *Escherichia coli* strain carrying a phosphoenolpyruvate: carbohydrate phosphotransferase system deletion by inactivating *arcA* and overexpressing the genes coding for glucokinase and galactose permease. *J. Mol. Microbiol. Biotechnol.* 13, 105–116. doi: 10.1159/000103602
- Ger, Y. M., Chen, S. L., Chiang, H. J., and Shiuan, D. (1994). A single Ser-180 mutation desensitizes feedback inhibition of the phenylalaninesensitive 3-deoxy-D-arabino-heptulosonate 7-phosphate (DAHP) synthetase in Escherichia coli. J. Biochem. 116, 986–990. doi: 10.1093/oxfordjournals.jbchem. a124657
- Ghosh, S., Chisti, Y., and Banerjee, U. C. (2012). Production of shikimic acid. Biotechnol. Adv. 30, 1425–1431. doi: 10.1016/j.biotechadv.2012.03.001
- Graf, M., Zieringer, J., Haas, T., Nieß, A., Blombach, B., and Takors, R. (2018). Physiological response of Corynebacterium glutamicum to increasingly nutrient-rich growth conditions. Front. Microbiol. 9:2058. doi: 10.3389/fmicb. 2018.02058
- Gu, P., Fan, X., Liang, Q., Qi, Q., and Li, Q. (2017). Novel technologies combined with traditional metabolic engineering strategies facilitate the construction of shikimate-producing *Escherichia coli. Microb. Cell Fact* 16:167. doi: 10.1186/ s12934-017-0773-y

- Hashiro, S., Mitsuhashi, M., and Yasueda, H. (2019). High copy number mutants derived from *Corynebacterium glutamicu*m cryptic plasmid pAM330 and copy number control. *J. Biosci. Bioeng.* 127, 529–538. doi: 10.1016/j.jbiosc.2018. 10.012
- Hirasawa, T., and Wachi, M. (2017). Glutamate fermentation-2: mechanism of L-Glutamate overproduction in Corynebacterium glutamicum. Adv. Biochem. Eng. Biotechnol. 159, 57–72. doi: 10.1007/10_2016_26
- Huccetogullari, D., Luo, Z. W., and Lee, S. Y. (2019). Metabolic engineering of microorganisms for production of aromatic compounds. *Microb. Cell Fact* 18:41. doi: 10.1186/s12934-019-1090-4
- Ikeda, M. (2006). Towards bacterial strains overproducing L-tryptophan and other aromatics by metabolic engineering. Appl. Microbiol. Biotechnol. 69, 615–626. doi: 10.1007/s00253-005-0252-y
- Ikeda, M. (2017). Lysine fermentation: history and genome breeding. Adv. Biochem. Eng. Biotechnol. 159, 73–102. doi: 10.1007/10_2016_27
- Jiang, M., and Zhang, H. (2016). Engineering the shikimate pathway for biosynthesis of molecules with pharmaceutical activities in E. coli. Curr. Opin. Biotechnol. 42, 1–6. doi: 10.1016/j.copbio.2016.01.016
- Jorge, J. M., Nguyen, A. Q., Pérez-García, F., Kind, S., and Wendisch, V. F. (2017). Improved fermentative production of gamma-aminobutyric acid via the putrescine route: Systems metabolic engineering for production from glucose, amino sugars, and xylose. *Biotechnol. Bioeng.* 114, 862–873. doi: 10.1002/bit. 26211
- Kanda, Y. (2013). Investigation of the freely available easy-to-use software 'EZR' for medical statistics. Bone Marrow Transplant. 48, 452–458. doi: 10.1038/bmt. 2012.244
- Käß, F., Junne, S., Neubauer, P., Wiechert, W., and Oldiges, M. (2014).
 Process inhomogeneity leads to rapid side product turnover in cultivation of Corynebacterium glutamicum. Microb. Cell. Fact 13:6. doi: 10.1186/1475-2859-13-6
- Khare, S. K., Pandey, A., and Larroche, C. (2015). Current perspectives in enzymatic saccharification of lignocellulosic biomass. *Biochem. Eng. J.* 102, 38–44. doi: 10.1016/j.bej.2015.02.033
- Kim, H. T., Baritugo, K., Hyun, S. M., Khang, T. U., Sohn, Y. J., Kang, K. H., et al. (2020). Development of metabolically engineered *Corynebacterium glutamicum* for enhanced production of cadaverine and its use for the synthesis of biopolyamide 510. ACS Sus. Chem. Eng. 8, 129–138. doi: 10.1021/acssuschemeng. 9b04693
- Kogure, T., and Inui, M. (2018). Recent advances in metabolic engineering of Corynebacterium glutamicum for bioproduction of value-added aromatic chemicals and natural products. Appl. Microbiol. Biotechnol. 102, 8685–8705. doi: 10.1007/s00253-018-9289-6
- Kogure, T., Kubota, T., Suda, M., Hiraga, K., and Inui, M. (2016). Metabolic engineering of Corynebacterium glutamicum for shikimate overproduction by growth-arrested cell reaction. Metab. Eng. 38, 204–216. doi: 10.1016/j.ymben. 2016.08.005
- Lee, J. H., and Wendisch, V. F. (2017). Biotechnological production of aromatic compounds of the extended shikimate pathway from renewable biomass. J. Biotechnol. 257, 211–221. doi: 10.1016/j.jbiotec.2016.11.016
- Li, Q., Yang, M. H., Wang, D., Li, W. L., Wu, Y., Zhang, Y. J., et al. (2010). Efficient conversion of crop stalk wastes into succinic acid production by Actinobacillus succinogenes. Bioresour. Technol. 101, 3292–3294. doi: 10.1016/j.biortech.2009. 12.064
- Liu, A., Liu, Z. Z., Zou, Z. M., Chen, S. Z., Xu, L. Z., and Yang, S. L. (2004). Synthesis of (+)-zeylenone from shikimic acid. *Tetrahedron* 60, 3689–3694. doi: 10.1016/j.tet.2004.02.066
- Liu, C. G., Xiao, Y., Xia, X. X., Zhao, X. Q., Peng, L., Srinophakun, P., et al. (2019). Cellulosic ethanol production: progress, challenges and strategies for solutions. *Biotechnol. Adv.* 37, 491–504. doi: 10.1016/j.biotechadv.2019.03.002
- Liu, Y. J., Li, P. P., Zhao, K. X., Wang, B. J., Jiang, C. Y., Drake, H. L., et al. (2008). Corynebacterium glutamicum contains 3-deoxy-D-arabino-heptulosonate 7phosphate synthases that display novel biochemical features. Appl. Environ. Microbiol. 74, 5497–5503. doi: 10.1128/AEM.00262-08
- Martinez, J. A., Bolivar, F., and Escalante, A. (2015). Shikimic acid production in Escherichia coli: from classical metabolic engineering strategies to omics applied to improve its production. Front. Bioeng. Biotechnol. 3:145. doi: 10.3389/fbioe. 2015.00145

- Matsuura, R., Kishida, M., Konishi, R., Hirata, Y., Adachi, N., Segawa, S., et al. (2019). Metabolic engineering to improve 1,5-diaminopentane production from cellobiose using β-glucosidase-secreting *Corynebacterium glutamicum*. *Biotechnol. Bioeng.* 116, 2640–2651. doi: 10.1002/bit.27082
- Noda, S., and Kondo, A. (2017). Recent advances in microbial production of aromatic chemicals and derivatives. *Trends Biotechnol.* 35, 785–796. doi: 10. 1016/j.tibtech.2017.05.006
- Ohnishi, J., Katahira, R., Mitsuhashi, S., Kakita, S., and Ikeda, M. (2005). A novel gnd mutation leading to increased L-lysine production in *Corynebacterium* glutamicum. FEMS Microbiol Lett. 242, 265–274. doi: 10.1016/j.femsle.2004. 11.014
- Pérez-García, F., and Wendisch, V. F. (2018). Transport and metabolic engineering of the cell factory *Corynebacterium glutamicum*. *FEMS Microbiol. Lett.* 365:fny166. doi: 10.1093/femsle/fny166
- Rawat, G., Tripathi, P., and Saxena, R. K. (2013). Expanding horizons of shikimic acid. Recent progresses in production and its endless frontiers in application and market trends. *Appl. Microbiol. Biotechnol.* 97, 4277–4287. doi: 10.1007/ s00253-013-4840-y
- Rodriguez, A., Martínez, J. A., Báez-Viveros, J. L., Flores, N., Hernández-Chávez, G., Ramírez, O. T., et al. (2013). Constitutive expression of selected genes from the pentose phosphate and aromatic pathways increases the shikimic acid yield in high-glucose batch cultures of an *Escherichia coli* strain lacking PTS and pykF. *Microb. Cell Fact* 12:86. doi: 10.1186/1475-2859-12-86
- Stansen, C., Uy, D., Delaunay, S., Eggeling, L., Goergen, J. L., and Wendisch, V. F. (2005). Characterization of a Corynebacterium glutamicum lactate utilization operon induced during temperature-triggered glutamate production. Appl. Environ. Microbiol. 71, 5920–5928. doi: 10.1128/AEM.71.10.5920-5928.2005
- Tanaka, T., Kawabata, H., Ogino, C., and Kondo, A. (2011). Creation of a cellooligosaccharide-assimilating *Escherichia coli* strain by displaying active beta-glucosidase on the cell surface via a novel anchor protein. *Appl. Environ. Microbiol.* 77, 6265–6270. doi: 10.1128/AEM.00459-11
- Tauch, A. (2005). "Native plasmids of amino acid-producing Corynebacteria," in Handbook of Corynebacterium glutamicum, eds L. Eggeling and M. Bott (Boca Raton, FL: CRC Press), 57–75. doi: 10.1201/9781420039696.ch4
- Van Dyk, J., and Pletschke, B. (2012). A review of lignocellulose bioconversion using enzymatic hydrolysis and synergistic cooperation between enzymes factors affecting enzymes, conversion and synergy. *Biotechnol. Adv.* 30, 1458–1480. doi: 10.1016/j.biotechadv.2012.03.002
- Vogt, M., Brüsseler, C., Ooyen, J. V., Bott, M., and Marienhagen, J. (2016).Production of 2-methyl-1-butanol and 3-methyl-1-butanol in engineered Corynebacterium glutamicum. Metab. Eng. 38, 436–445. doi: 10.1016/j.ymben. 2016.10.00

- Wendisch, V. F., Mindt, M., and Pérez-García, F. (2018). Biotechnological production of mono- and diamines using bacteria: recent progress, applications, and perspectives. Appl. Microbiol. Biotechnol. 102, 3583–3594. doi: 10.1007/ s00253-018-8890-z
- Ximenes, E., Kim, Y., Mosier, N., Dien, B., and Ladisch, M. (2011). Deactivation of cellulases by phenols. *Enz. Microb. Technol.* 48, 54–60. doi: 10.1016/j.enzmictec. 2010.09.006
- Yim, S. S., An, S. J., Choi, J. W., Ryu, A. J., and Jeong, K. J. (2014). High-level secretory production of recombinant single-chain variable fragment (scFv) in Corynebacterium glutamicum. Appl. Microbiol. Biotechnol. 98, 273–284. doi: 10.1007/s00253-013-5315-x
- Yim, S. S., An, S. J., Kang, M., Lee, J., and Jeong, K. J. (2013). Isolation of fully synthetic promoters for high-level gene expression in *Corynebacterium glutamicum*. *Biotechnol. Bioeng*. 110, 2959–2969. doi: 10.1002/bit.24954
- Zhang, B., Liu, Z. Q., Liu, C., and Zheng, Y. G. (2016). Application of CRISPRi in Corynebacterium glutamicum for shikimic acid production. Biotechnol. Lett. 38, 2153–2161. doi: 10.1007/s10529-016-2207-
- Zhang, B., Jiang, C. Y., Liu, Y. M., Liu, C., and Liu, S. J. (2015a). Engineering of a hybrid route to enhance shikimic acid production in *Corynebacterium glutamicum*. *Biotechnol. Lett.* 37, 1861–1868. doi: 10.1007/s10529-015-1852-y
- Zhang, B., Zhou, N., Liu, Y. M., Liu, C., Lou, C. B., Jiang, C. Y., et al. (2015b). Ribosome binding site libraries and pathway modules for shikimic acid synthesis with Corynebacterium glutamicum. Microb. Cell Fact 14:71. doi: 10. 1186/s12934-015-0254-
- Zhang, C., Zhang, J., Kang, Z., Du, G., and Chen, J. (2015). Rational engineering of multiple module pathways for the production of L-phenylalanine in Corynebacterium glutamicum. J. Ind. Microbiol. Biotechnol. 42, 787–797. doi: 10.1007/s10295-015-1593-x
- Zhao, X., Zheng, Z., Cai, Y., Zhao, Y., Zhang, Y., Gao, Y., et al. (2020). Accelerated biomethane production from lignocellulosic biomass: pretreated by mixed enzymes secreted by *Trichoderma viride* and *Aspergillus* sp. *Bioresour. Technol.* 309:123378. doi: 10.1016/j.biortech.2020.123378

Conflict of Interest: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

Copyright © 2020 Sato, Kishida, Nakano, Hirata and Tanaka. This is an open-access article distributed under the terms of the Creative Commons Attribution License (CC BY). The use, distribution or reproduction in other forums is permitted, provided the original author(s) and the copyright owner(s) are credited and that the original publication in this journal is cited, in accordance with accepted academic practice. No use, distribution or reproduction is permitted which does not comply with these terms.